

PUMPING FROM DEEP HOLES: DEVELOPING OPTIMIZED HYDRAULIC DESIGNS



Graz, 10. April 2024

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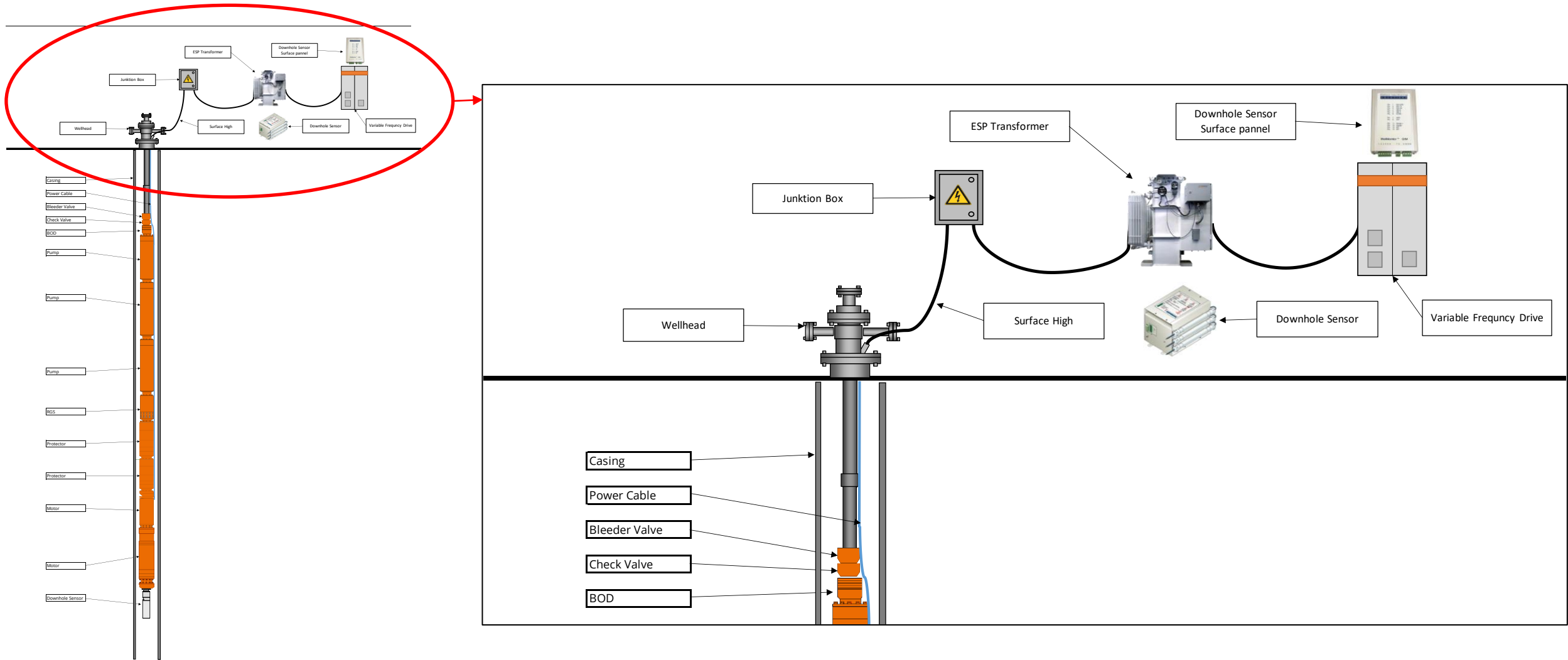


Stefan Höller

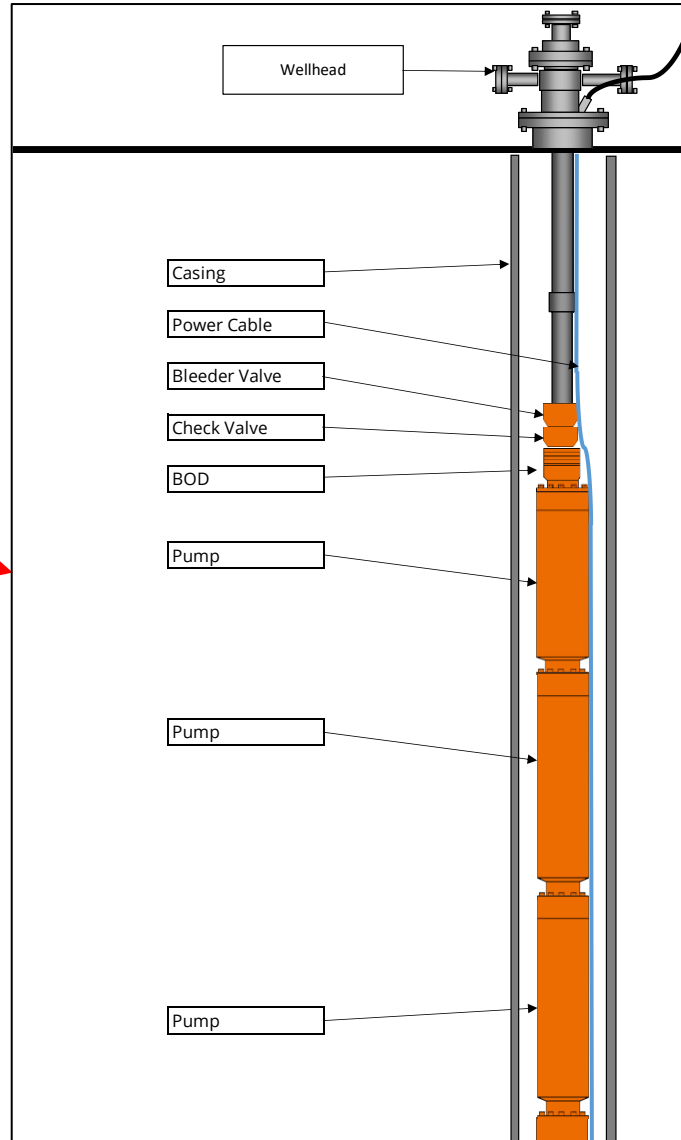
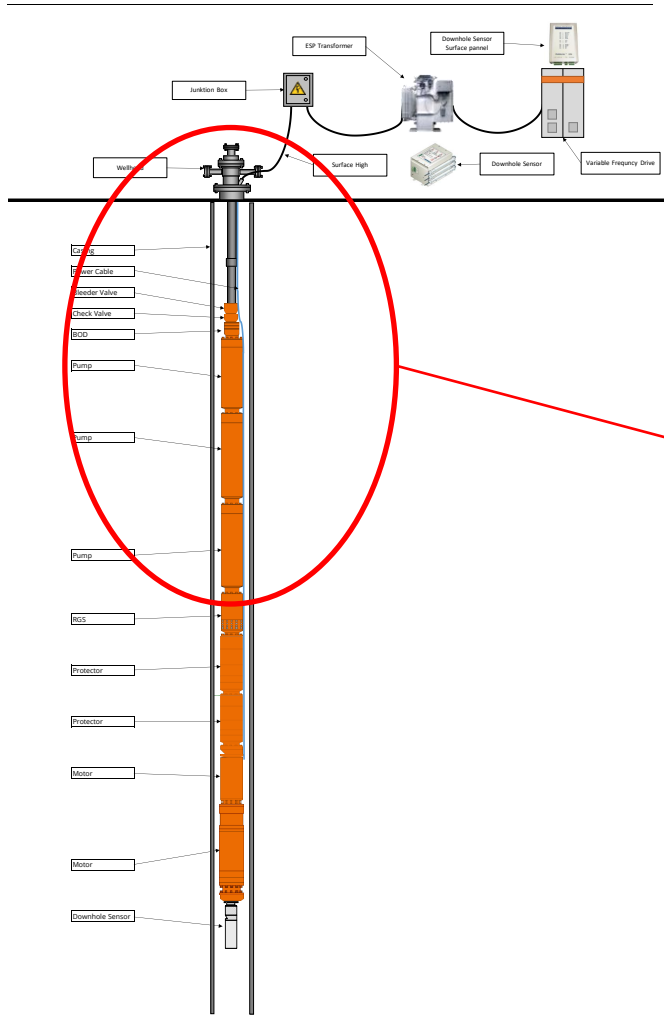
Senior Engineer
Stefan.Hoeller@JabergundPartner.com



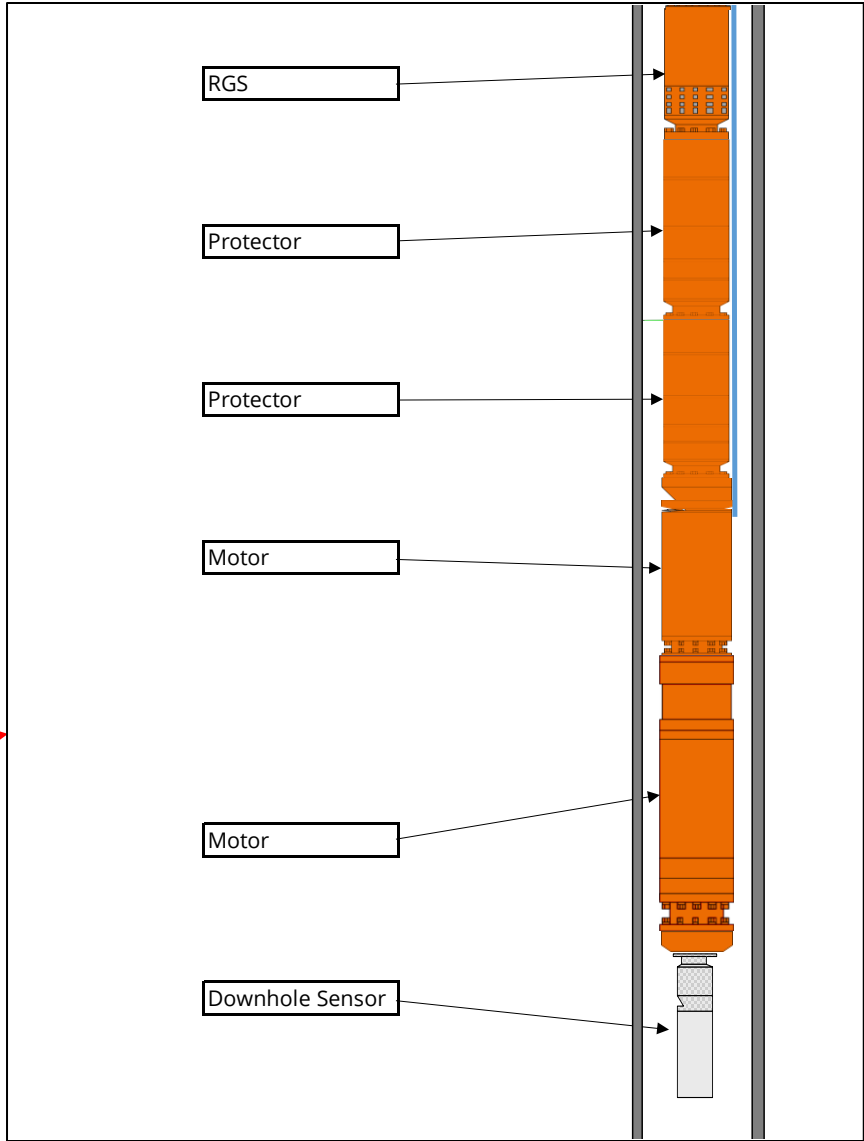
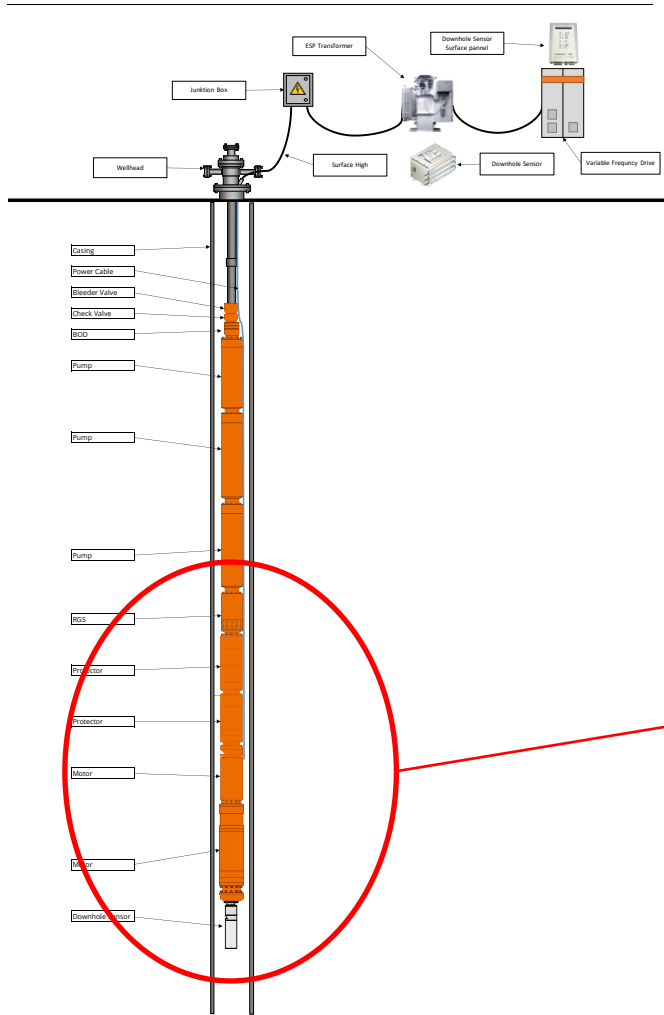
Typical Geothermal Installation - String Diagram



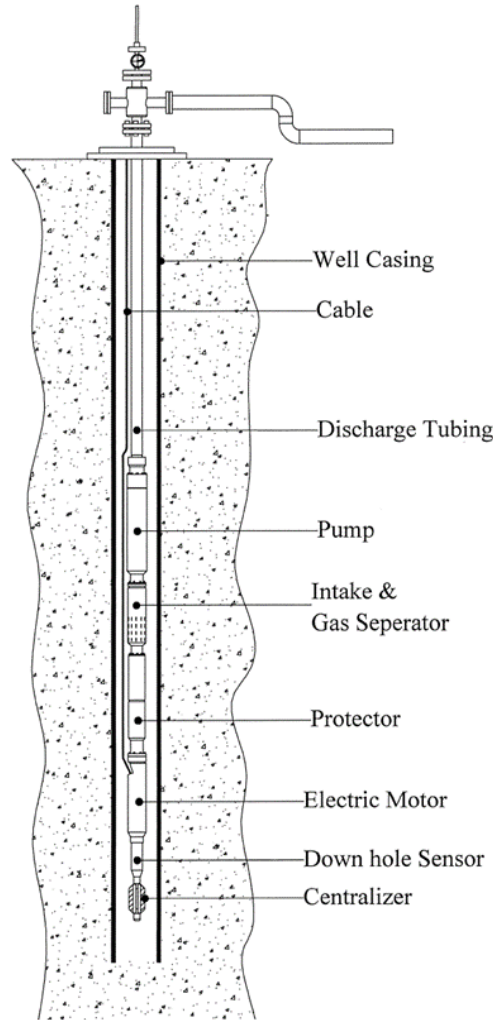
Typical Geothermal Installation - String Diagram



Typical Geothermal Installation - String Diagram



Typical Geothermal Installation



Casing size:

10-3/4" with liner or,
9-5/8" without liner

Maximum acceptable pump diameter 7.7"

8.75" pumps are too large
6.75" pump cannot deliver required
flow rate (36000BPD max)

Required production rates:

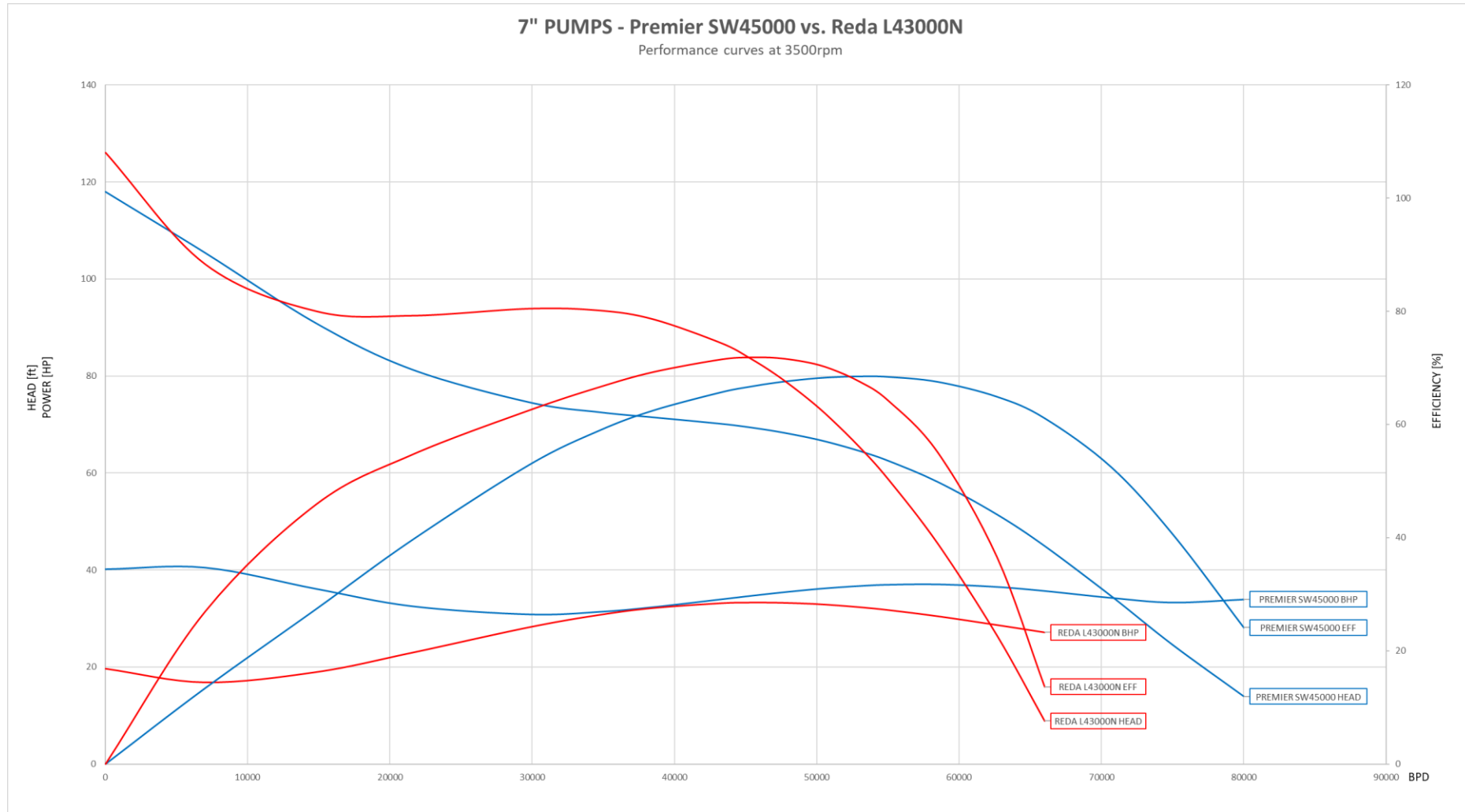
winter 45000-50000BPD / 82.8-92[l/s]
summer 15000-20000BPD / 27.6-36.8[l/s]

Production zone at 3000-4000m from surface

Pump landed at 600-1000m from surface



Pumps Available from Competition



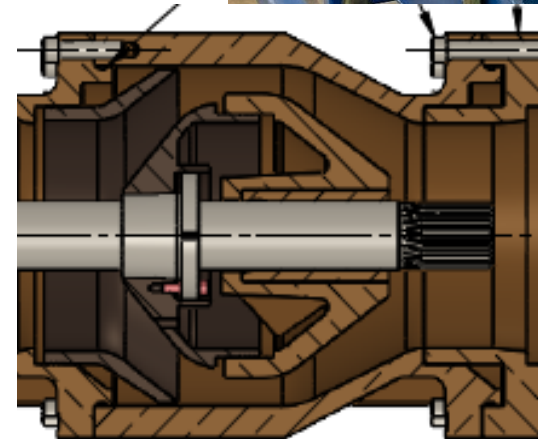
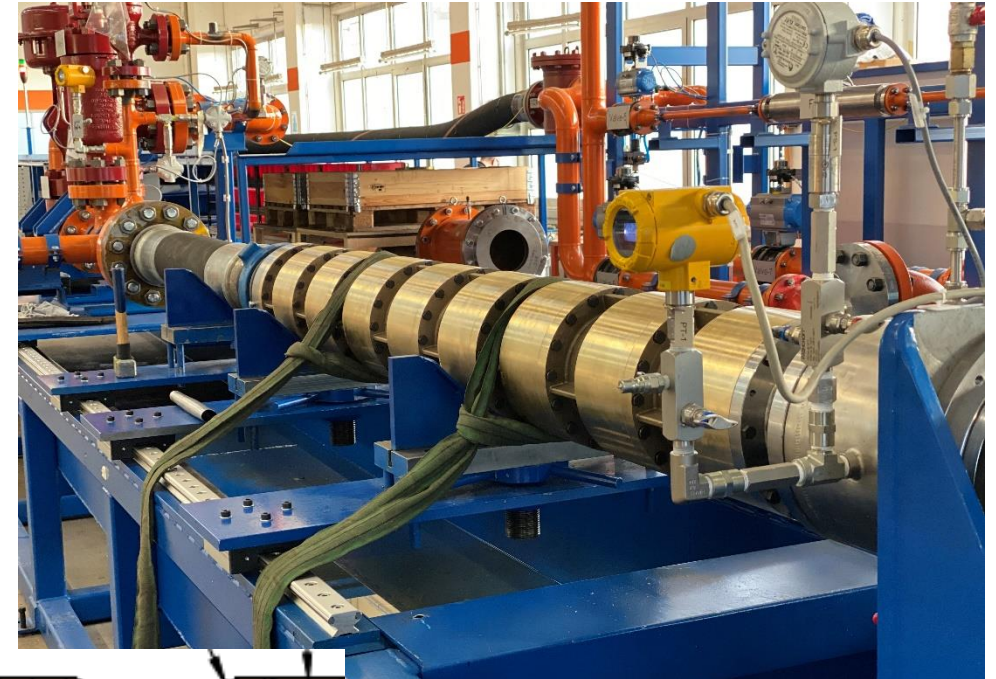
Initial Situation / Task / Goal

Hydraulic Specifications (n = 3500 rpm)

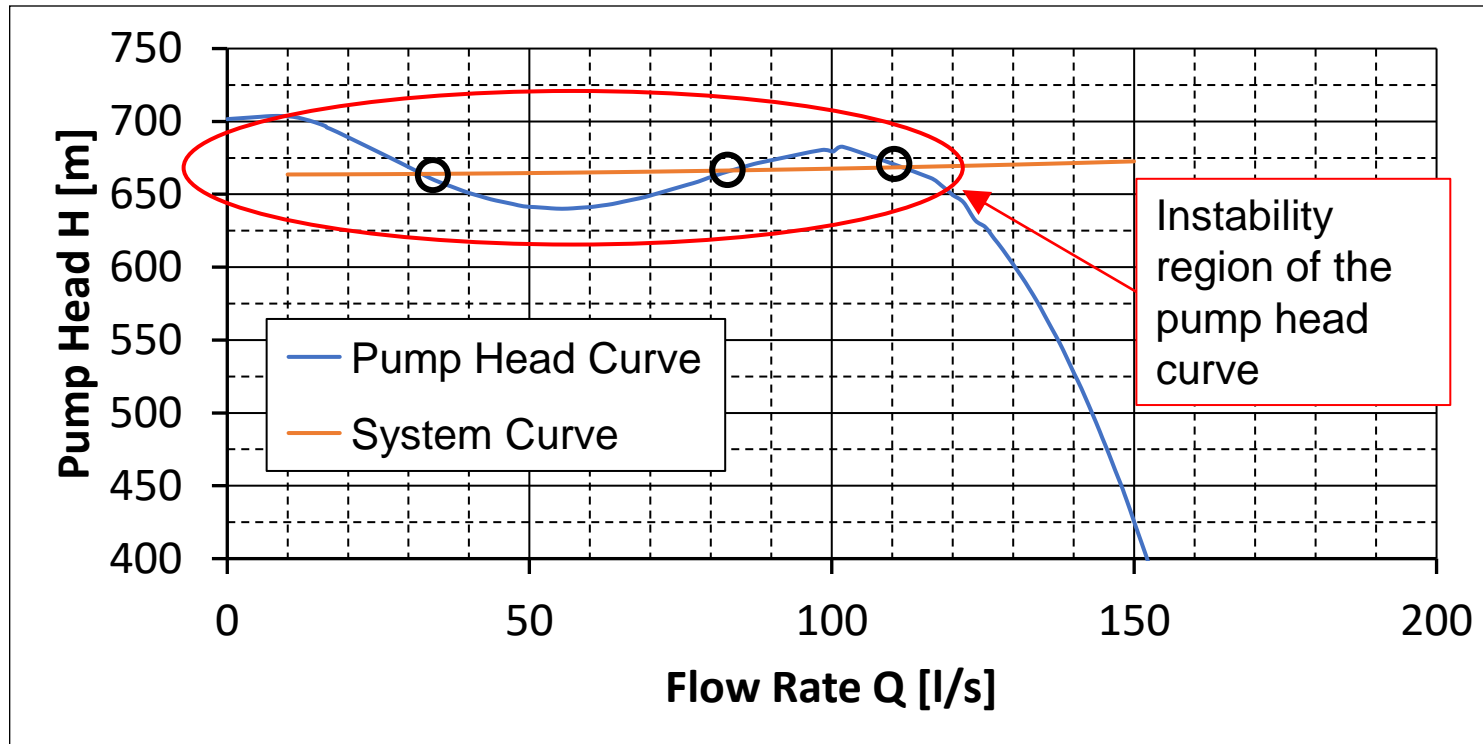
- Expected **head** per stage at BEP **25m**
- Flow rate at BEP **298m³/h or 45,000bpd**
- Expected efficiency at BEP would be close to 80%
- Continuously rising pump head is a must. Pump must be stable in whole range from no flow to no head conditions.
- No specifications concerning cavitation provided

Design specifications:

- Diffuser overall diameter [OD] must not bigger than **7-1/2" (190.5mm)**
- Max. **wet diameter D_a** to 172mm



Non-stable Pump Head Curve



System curve crosses the instability region:
multiple intersections at different flow rates possible

➔ Sudden jumps in flow rate can be described by multiple intersections of the pump head curve and the system resistance curve



Literature study / possible limitations

- $H_{BEP} = 25 \text{ m}$, $Q_{BEP} = 298 \text{ m}^3/\text{h}$ bzw 82.8 l/s , $n = 3500 \text{ rpm}$
- Max. wet diameter D_a to 172mm

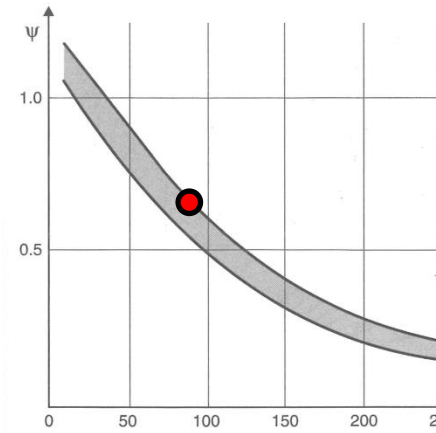
$$n_q = n \frac{\sqrt{Q_{BEP}}}{H_{BEP}^{3/4}} = 3500 \frac{\sqrt{0.0828}}{25^{3/4}} = 90$$

$$\psi = \frac{2 \cdot g \cdot H}{u^2} = \frac{2 \cdot 9.81 \cdot 25}{\left(0.1475 \cdot \pi \cdot \frac{3500}{60}\right)^2} = 0.67$$

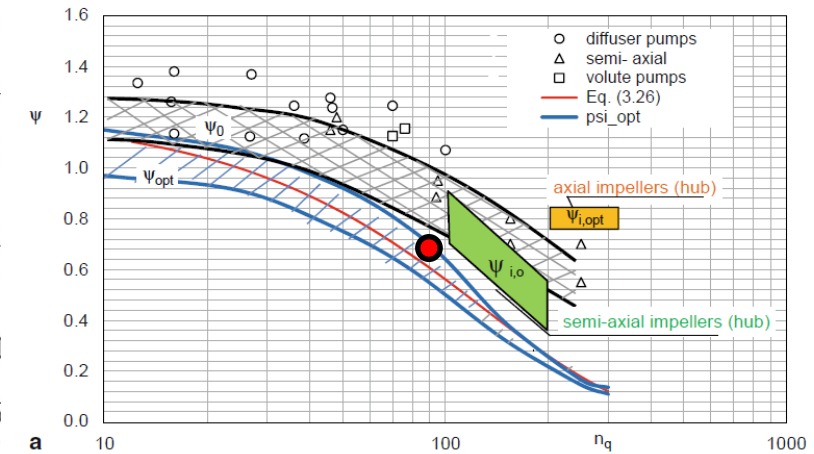
$\Psi = 0,67$ @ $n_q = 90$ can be treated as tough design specification since for both references it is on the upper limit curve;

Gülich mentions to take the lower limit curve if a stable head curve should be achieved

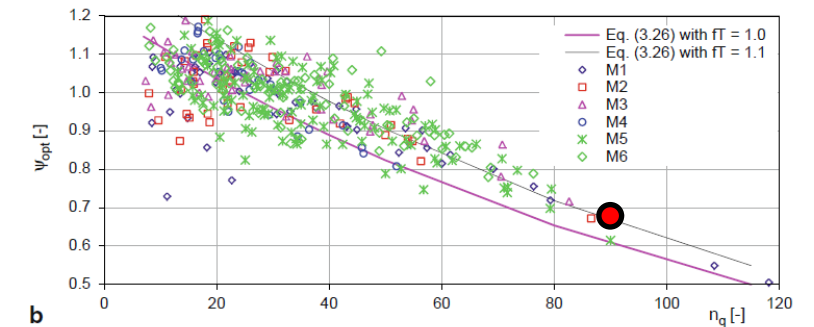
⇒ In our design experience, the maximum permissible impeller diameter for the given combination of Q, H and n is at the very low limit!



Source: Sulzer



a



b

Source: Gülich

A study of reference pumps from different competitors revealed that **no executed pump with a stable head curve** under these specifications ($Q_{BEP} = 298 \text{ m}^3/\text{h}$ @ $n = 3500 \text{ rpm}$ with $D_2 \sim 150 \text{ mm}$) and could be found.

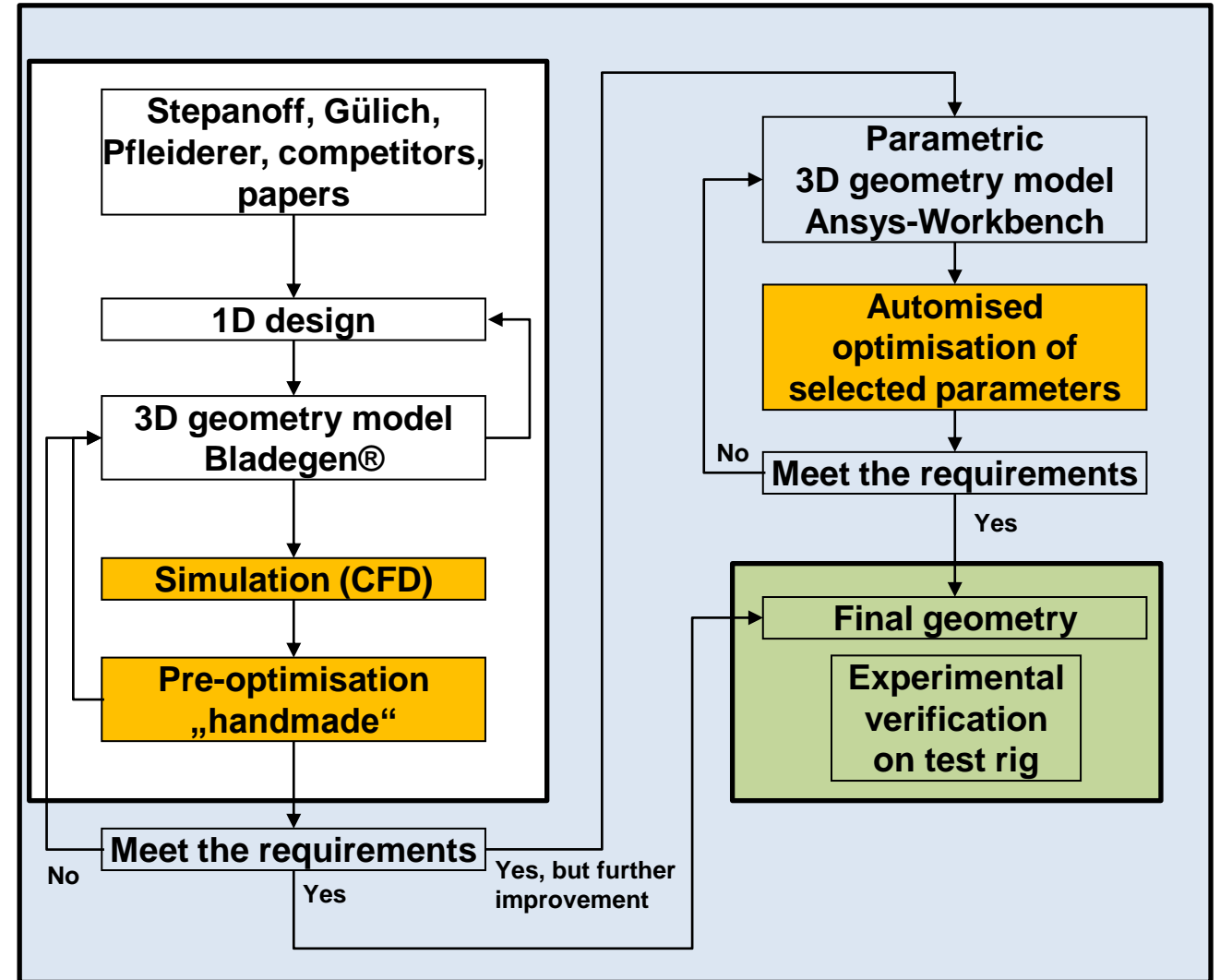
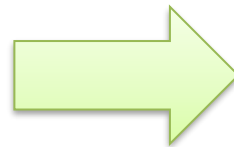


Hydraulic Design / Optimization Procedure

Challenges:

- No reliable design guidelines for mixed flow pump diffusers
- Hardly any references for the given design targets such as **head curve stability** and **limited size**
- Satisfying demanding design targets
- Many degrees of freedom

customized design procedure



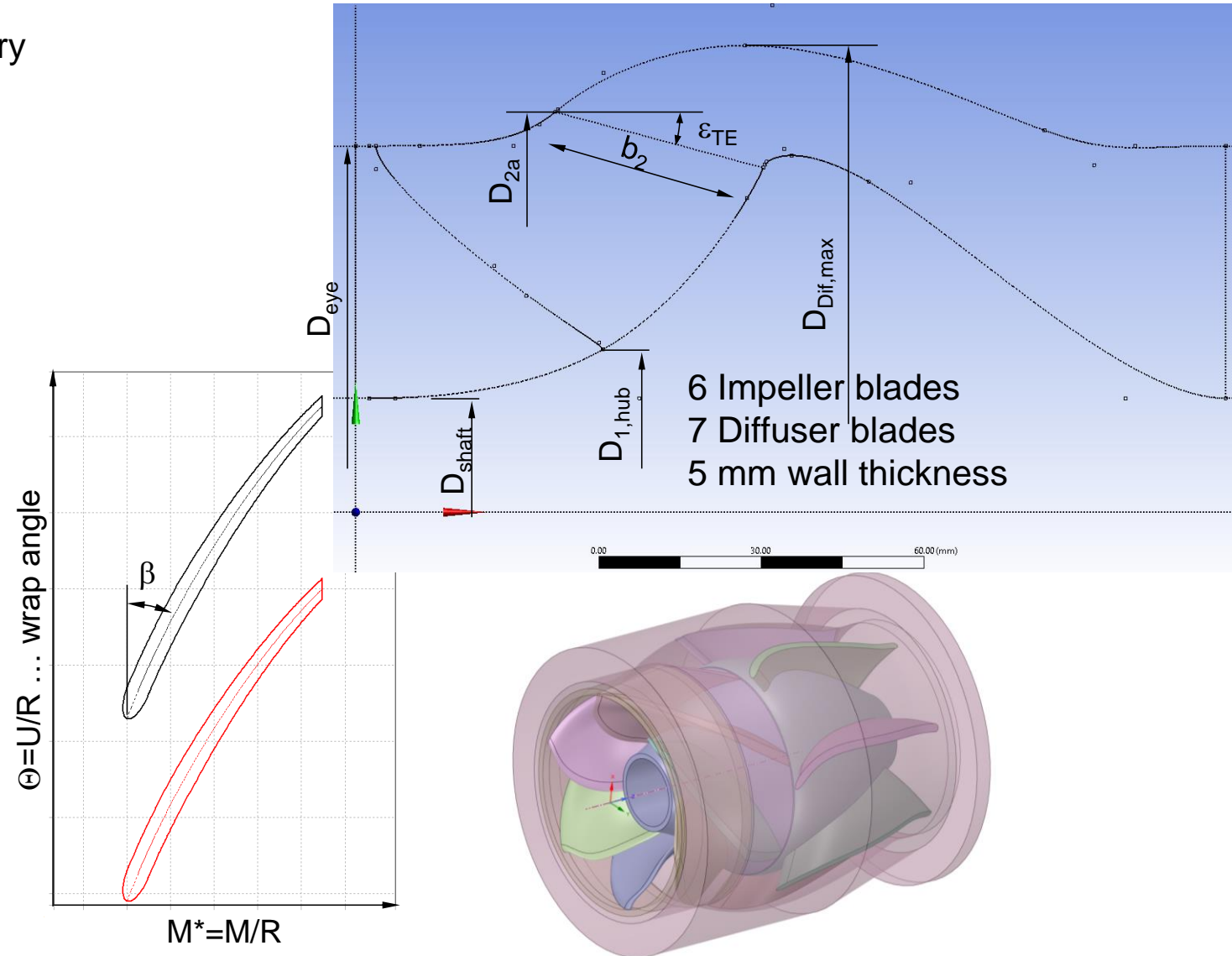
Parametric CAD-Model for Impeller and Diffuser

Parametric model for the complete hydraulic geometry

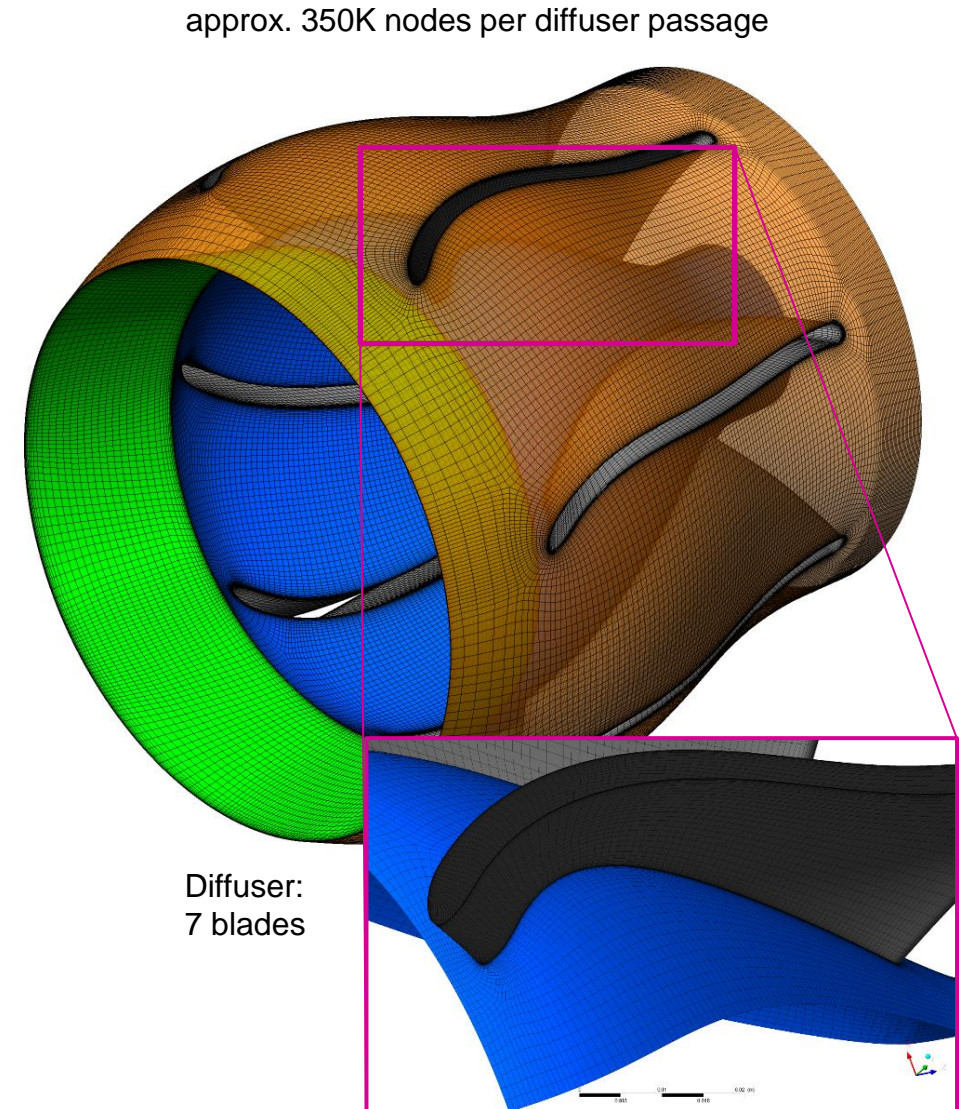
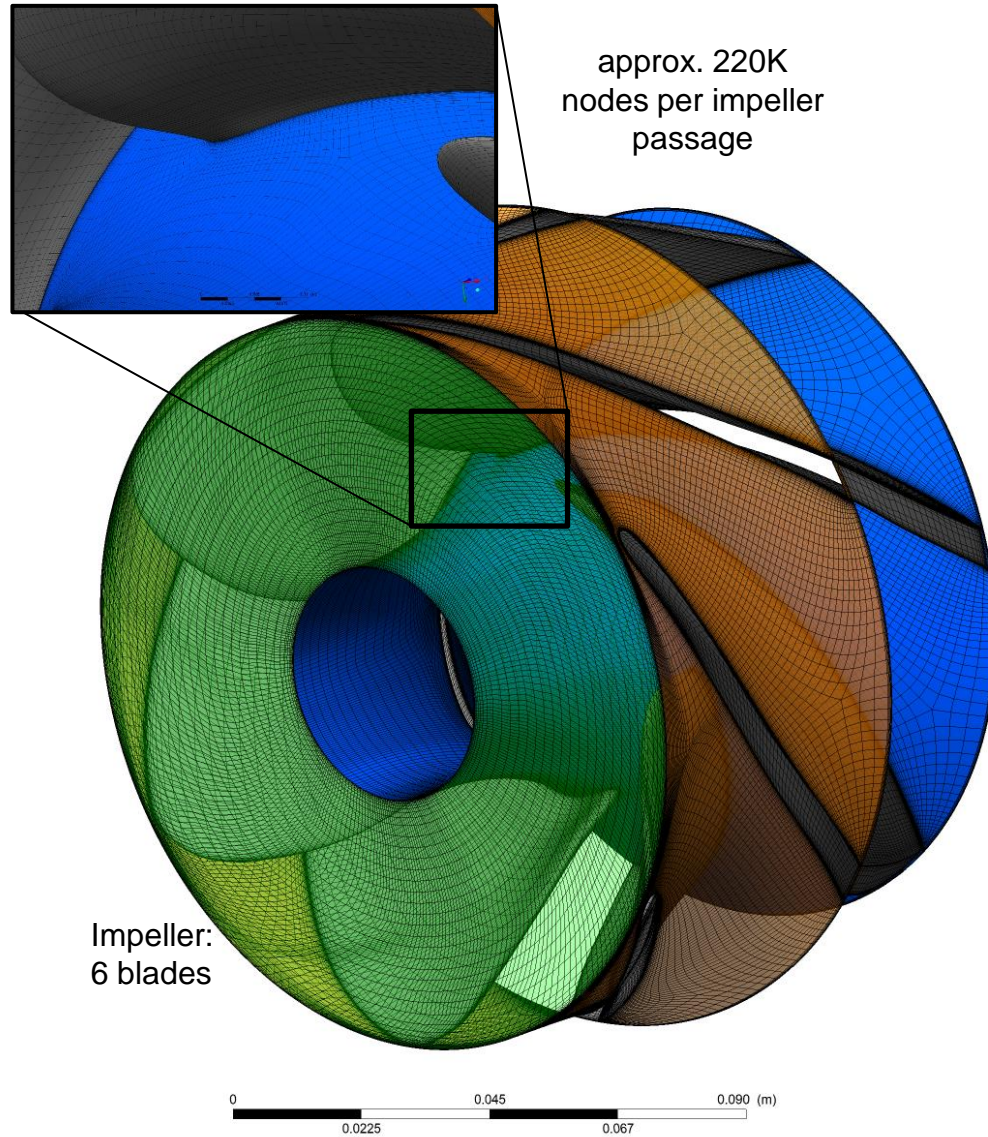
- meridional cross section
- blade shaping

more than 30 degrees of freedom was created.

- Multi-stage suitable; max. dimensions limited
- Minimization of remaining swirl at pump exit
- Smooth flow deceleration; Minimal flow separation but rapidly changing meridional curvature (limited diameter);
- Strong influence on head curve stability
- Sensitivity analysis followed by metamodel-assisted multi-objective evolutionary optimization



Numerical Meshes Impeller and Diffuser



CFD Setup

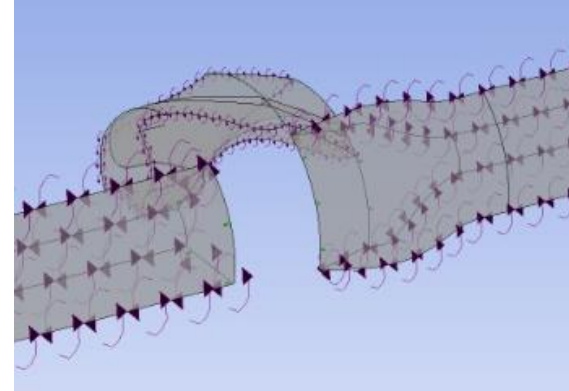
Steady State simulations for optimization

- Single passage models A and B
- Full 360° Model C for verification
- SST turbulence model
- Aggressive time step (speed up calculation time)
- Approx. 15 (A) / 30 (B) minutes on 4 CPU cores; 8 h (C) on 16 CPU cores
- more than thousand different geometries investigated; 5 operating points for each geometry (to prove head curve stability)

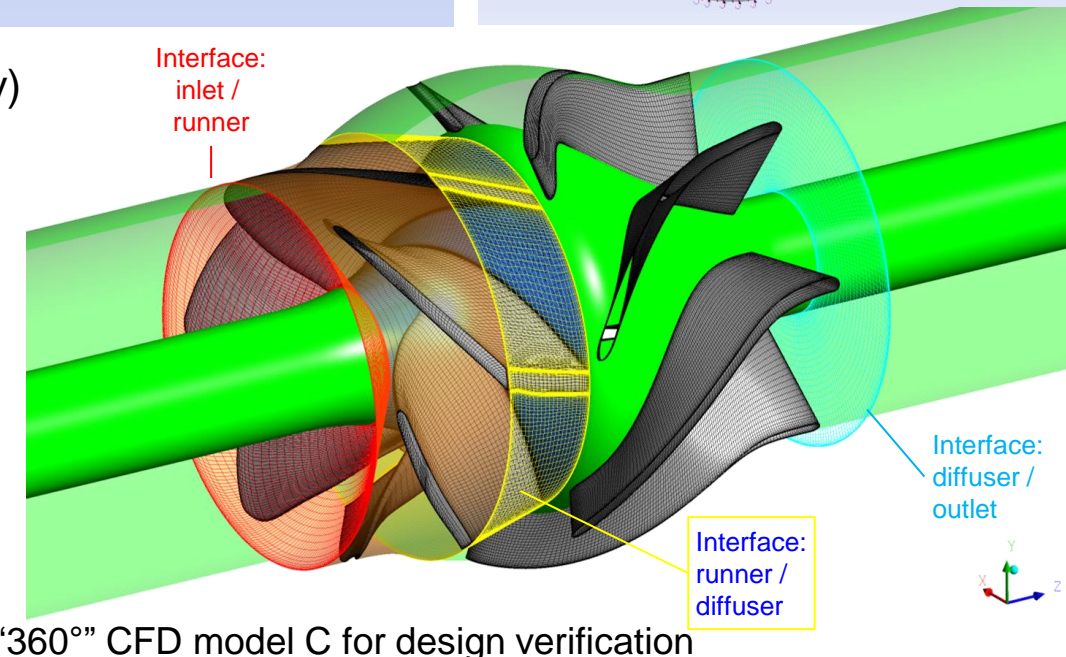
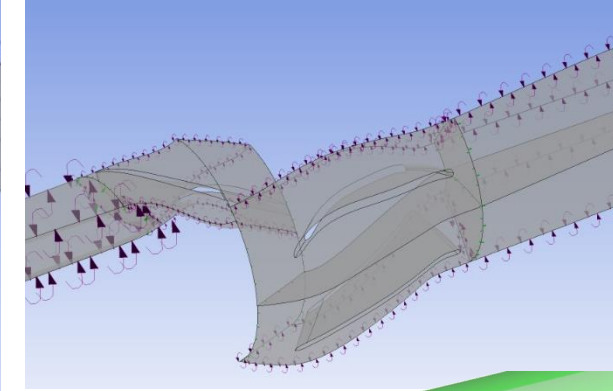
Transient simulations

- Full 360° model for all domains, SBES-SST turbulence model
- Before automated optimization + for final geometry
- Approx. 5 to 6 days on 16 CPU cores

“Impeller only” CFD model A
for impeller design process



“Simple” CFD model B
for diffuser design process



“360°” CFD model C for design verification



Post-Processing

$$H_{pump} = \frac{1}{\rho g} \left[\left(\frac{1}{4} \sum_{i=1}^4 p_i + \frac{\rho}{2} \left(\frac{Q}{A} \right)^2 \right) \Big|_{out} - \left(\frac{1}{4} \sum_{i=1}^4 p_i + \frac{\rho}{2} \left(\frac{Q}{A} \right)^2 \right) \Big|_{in} \right]$$

... Pump Head acc. ISO 9906

$$H_{pump} = \frac{1}{\rho g} \left[\frac{1}{A_{out}} \left(\int p \cdot dA \right) \Big|_{out} - \frac{1}{A_{in}} \left(\int p \cdot dA \right) \Big|_{in} \right] + \frac{\left(\frac{Q}{A_{out}} \right)^2 - \left(\frac{Q}{A_{in}} \right)^2}{2g}$$

... Pump Head CFD

$$\eta_{hydr} = \frac{P_{hydr}}{P_{mech}} = \frac{\rho \cdot g \cdot Q \cdot H_{pump}}{T_{Runner} \cdot \omega} =$$

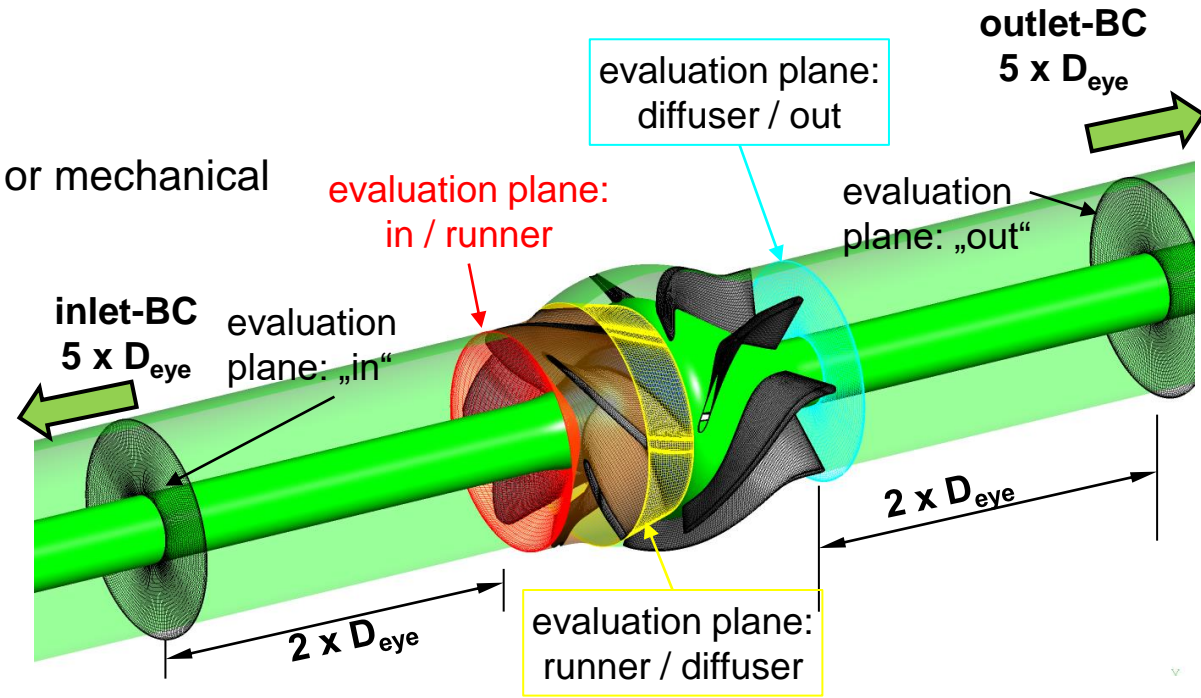
no leakage loss, disc friction or mechanical (bearing, sealing) losses

$$\rho \cdot g \cdot Q \cdot H_{pump}$$

$$\frac{H_{pump}}{(T_{RunnerBlades} + T_{RunnerHub} + T_{RunnerShroud}) \cdot \frac{2 \cdot \pi \cdot n}{60}}$$

$$\eta_{hydr} = \frac{H_{pump}}{H_{pump} + \sum H_L} =$$

$$\frac{H_{pump}}{H_{pump} + H_{L-inlet} + H_{L-runner} + H_{L-diffuser} + H_{L-outlet}}$$

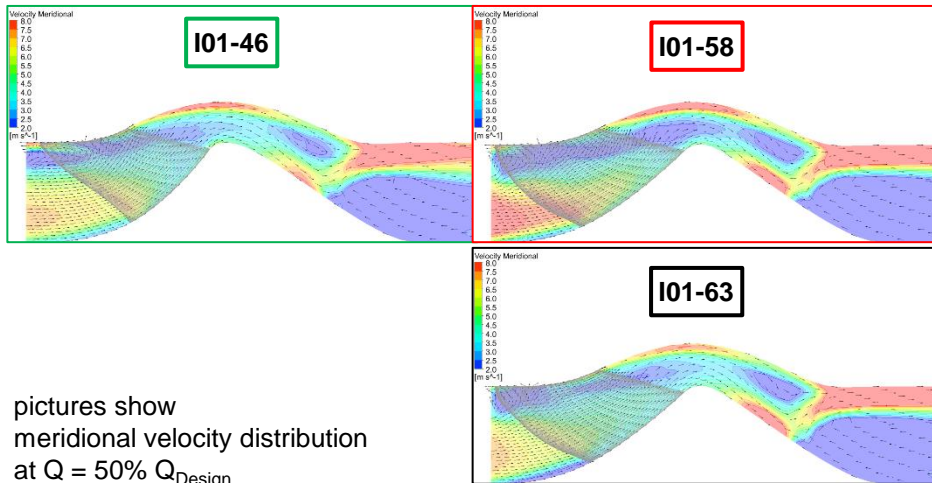
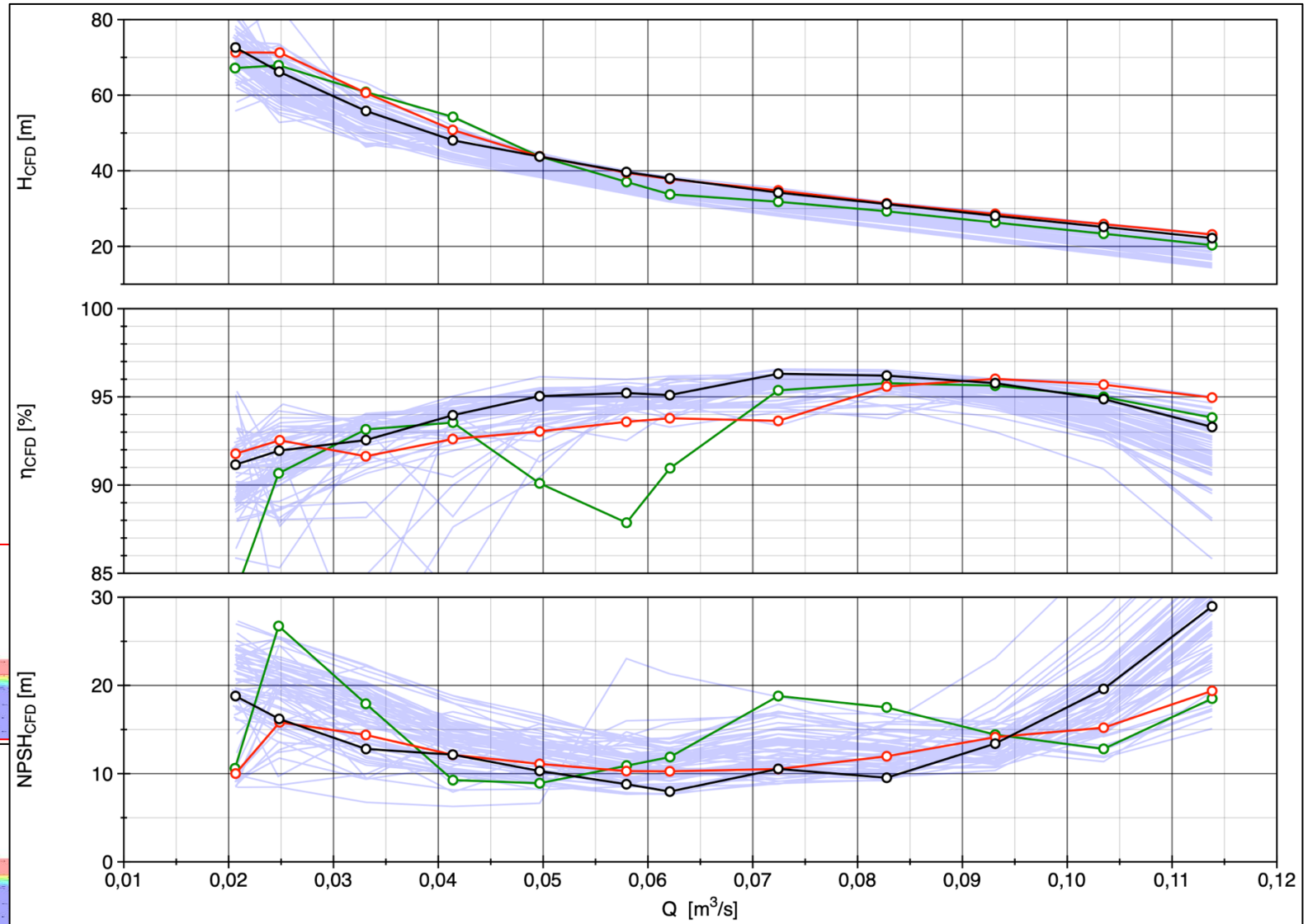


Selected Impeller Designs from Optimization Process

80 impeller designs were investigated further (out of approx. one thousand!);

Main focus on velocity distribution at impeller inlet and outlet at part load operation (stable head curve mandatory!)

3 examples were chosen in the design process for further diffuser design



pictures show meridional velocity distribution at $Q = 50\% Q_{\text{Design}}$



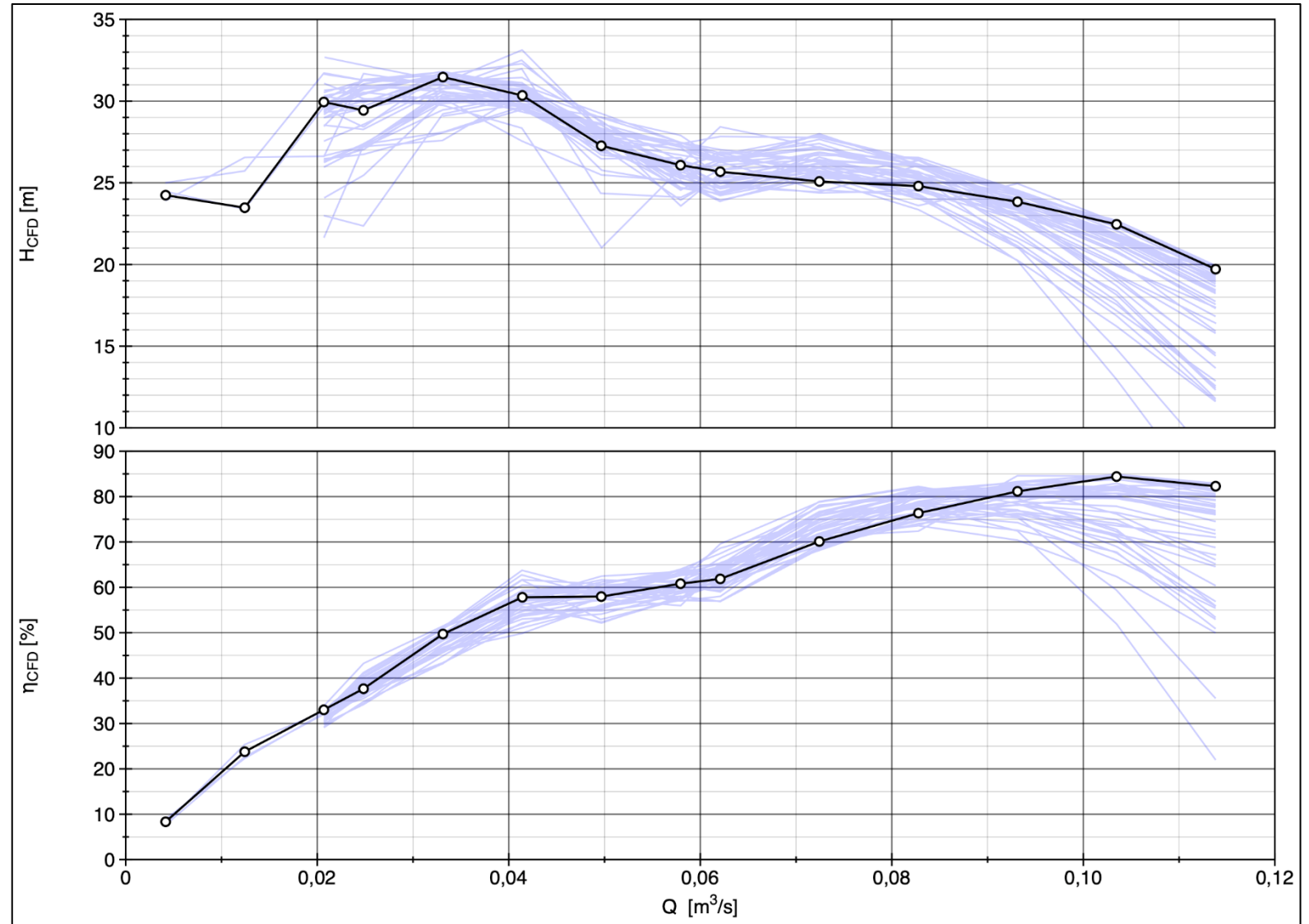
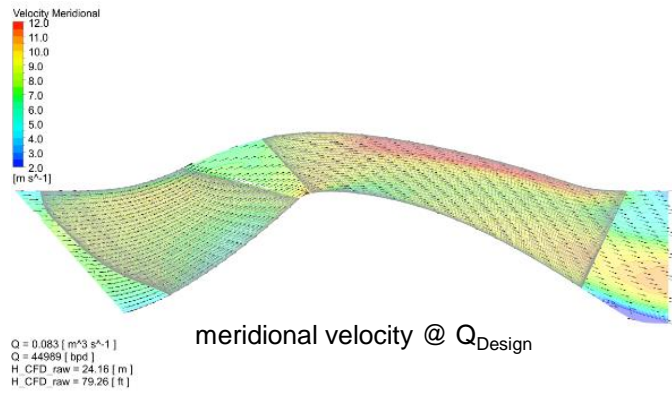
Selected Diffuser Design from Optimization Process

The most challenging task was to find an impeller / diffuser combination with a stable head curve.

It turned out that in part load an increase of pump head beyond 30 m is not possible.

At least down to a flowrate of $Q = 33 \text{ l/s}$ ($\cong 40\% Q_{\text{Design}}$) the numerical results of the optimized design show a stable head / flowrate behaviour.

To achieve this head curve stability the best efficiency point is shifted to a flow rate above Q_{Design} (approx. 120%)

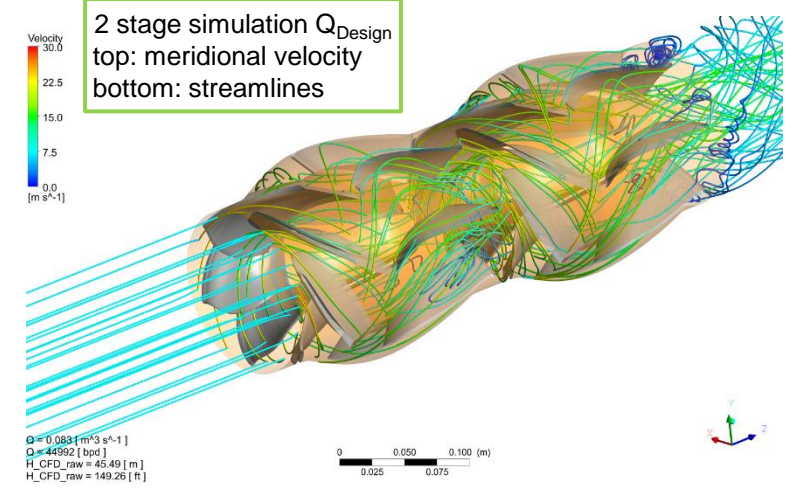
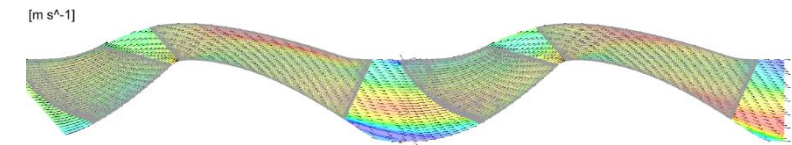
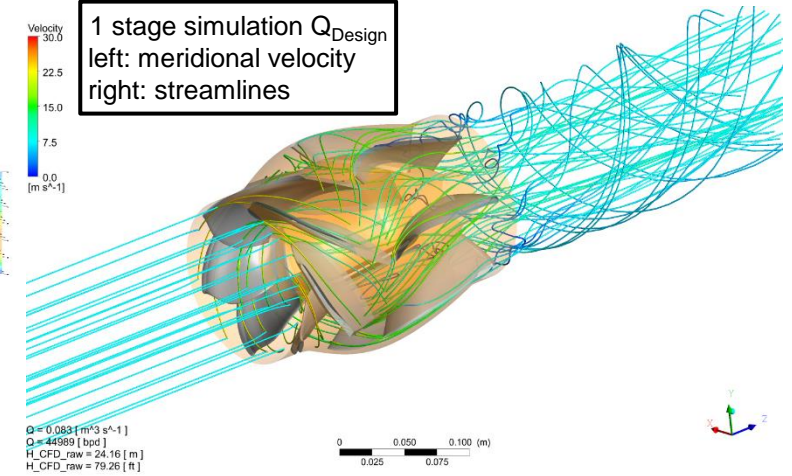
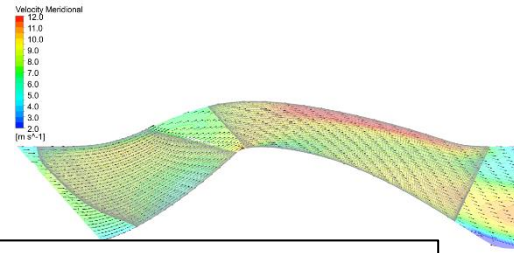
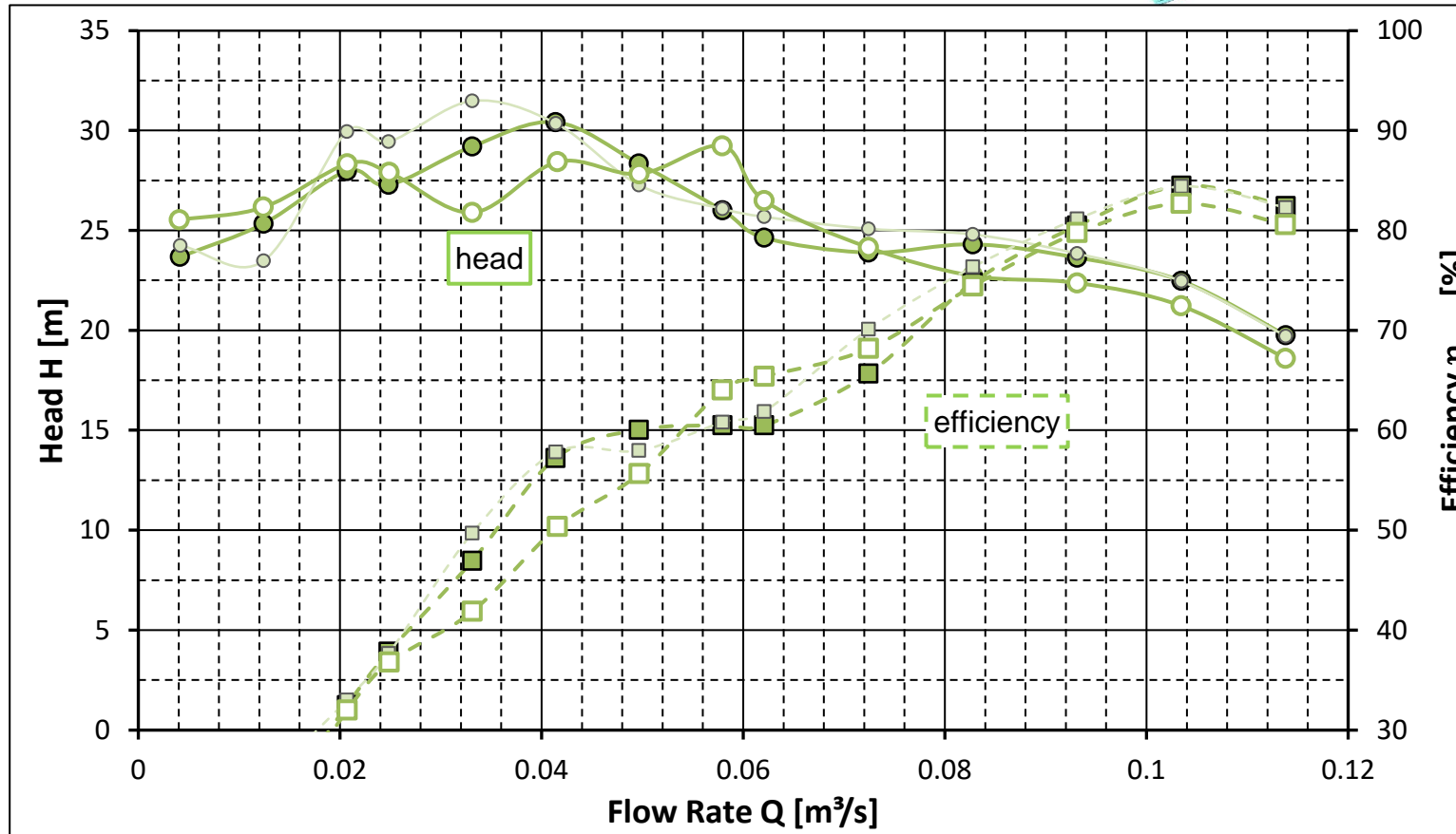


Comparison of different CFD-models

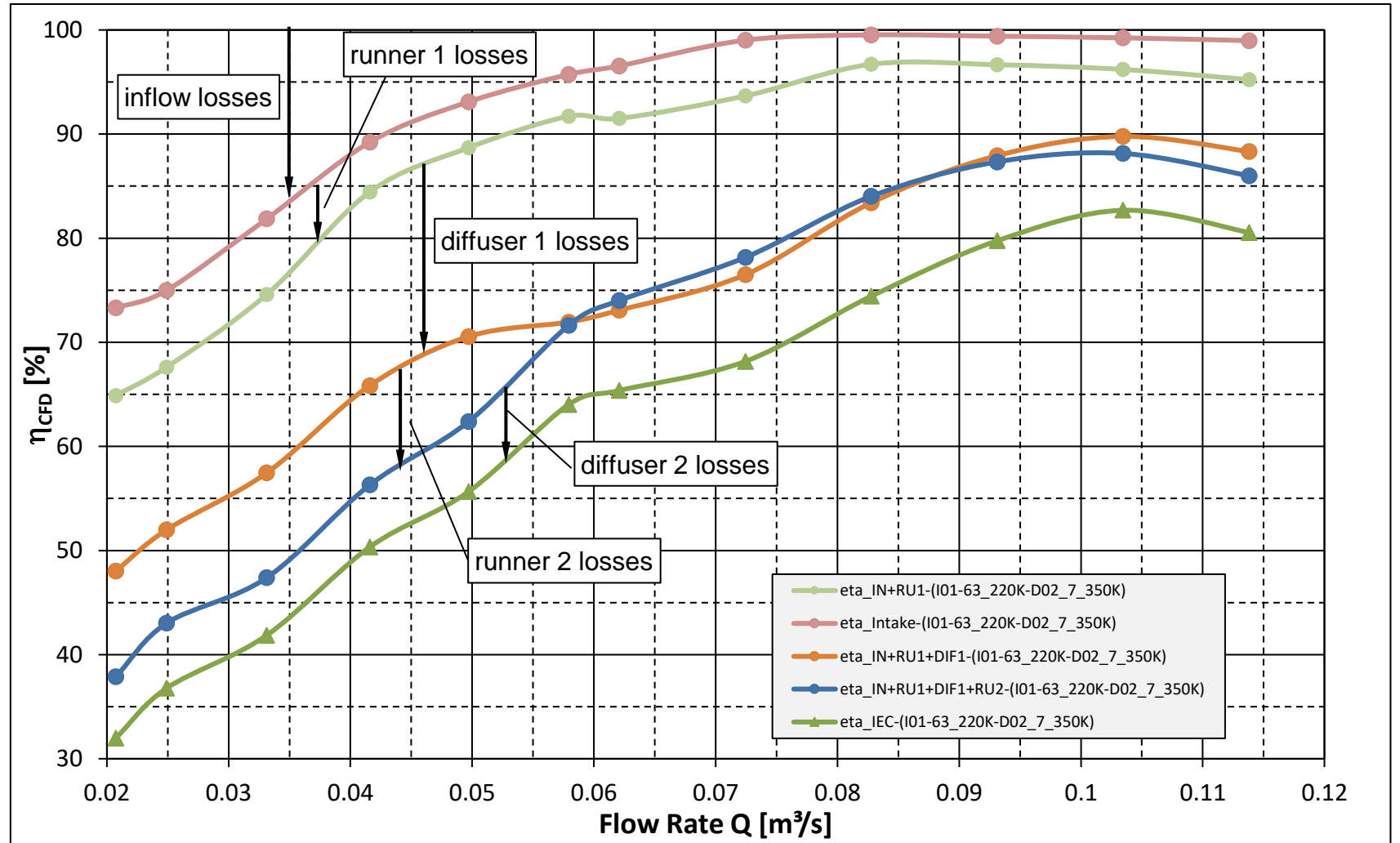
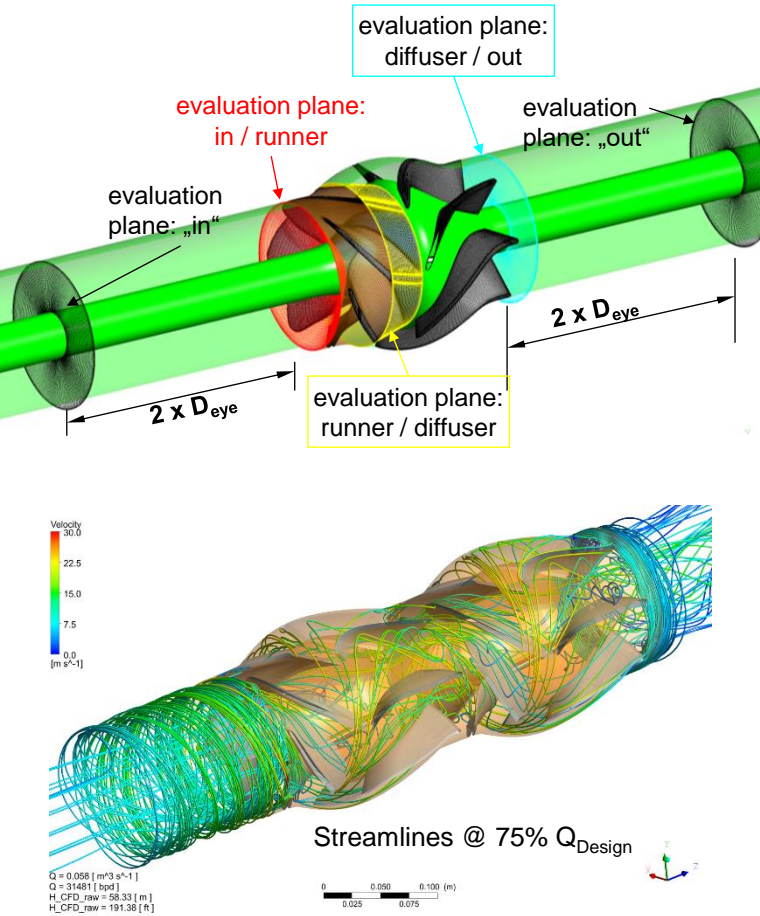
Bright green: simple model;

Coloured markers with black lines: full model 1 stage;

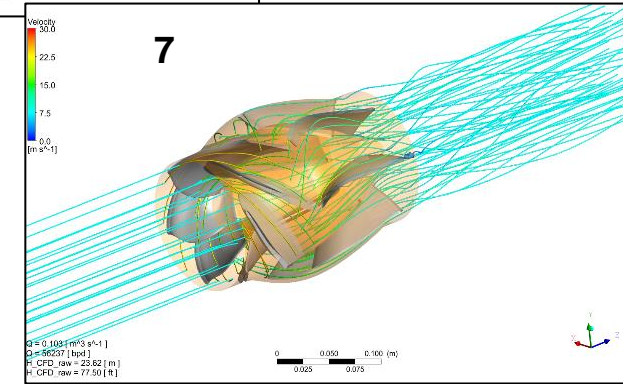
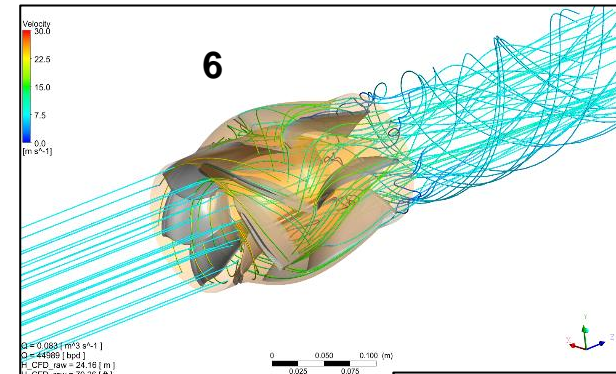
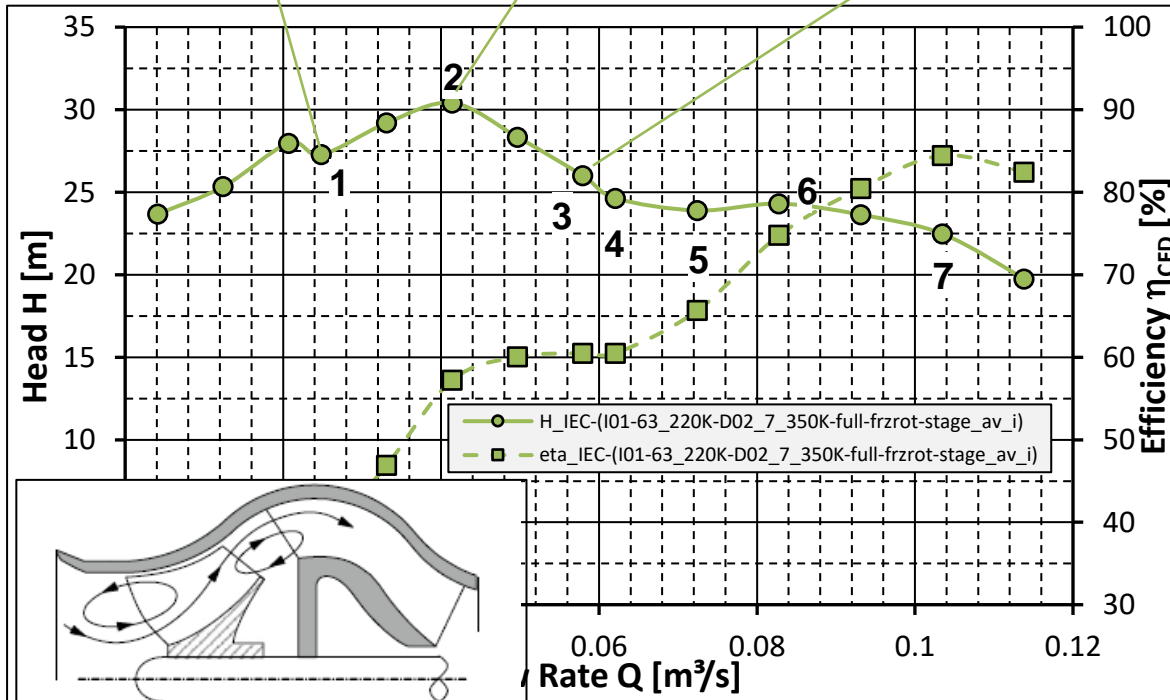
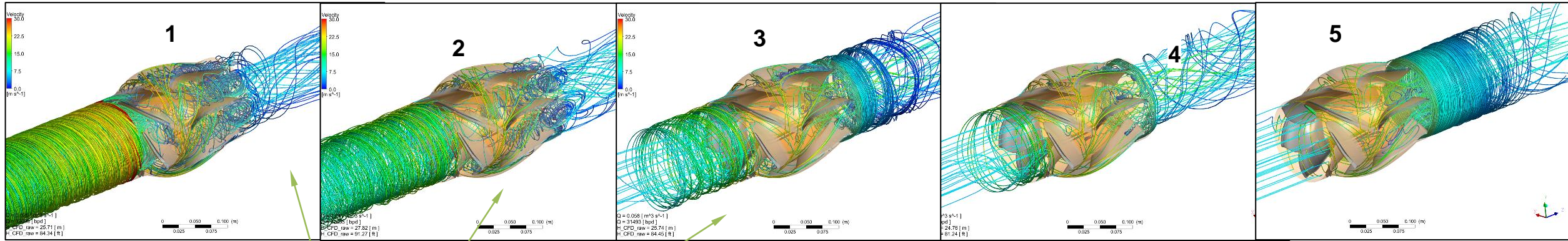
Blank markers with green lines: full model 2 stage;



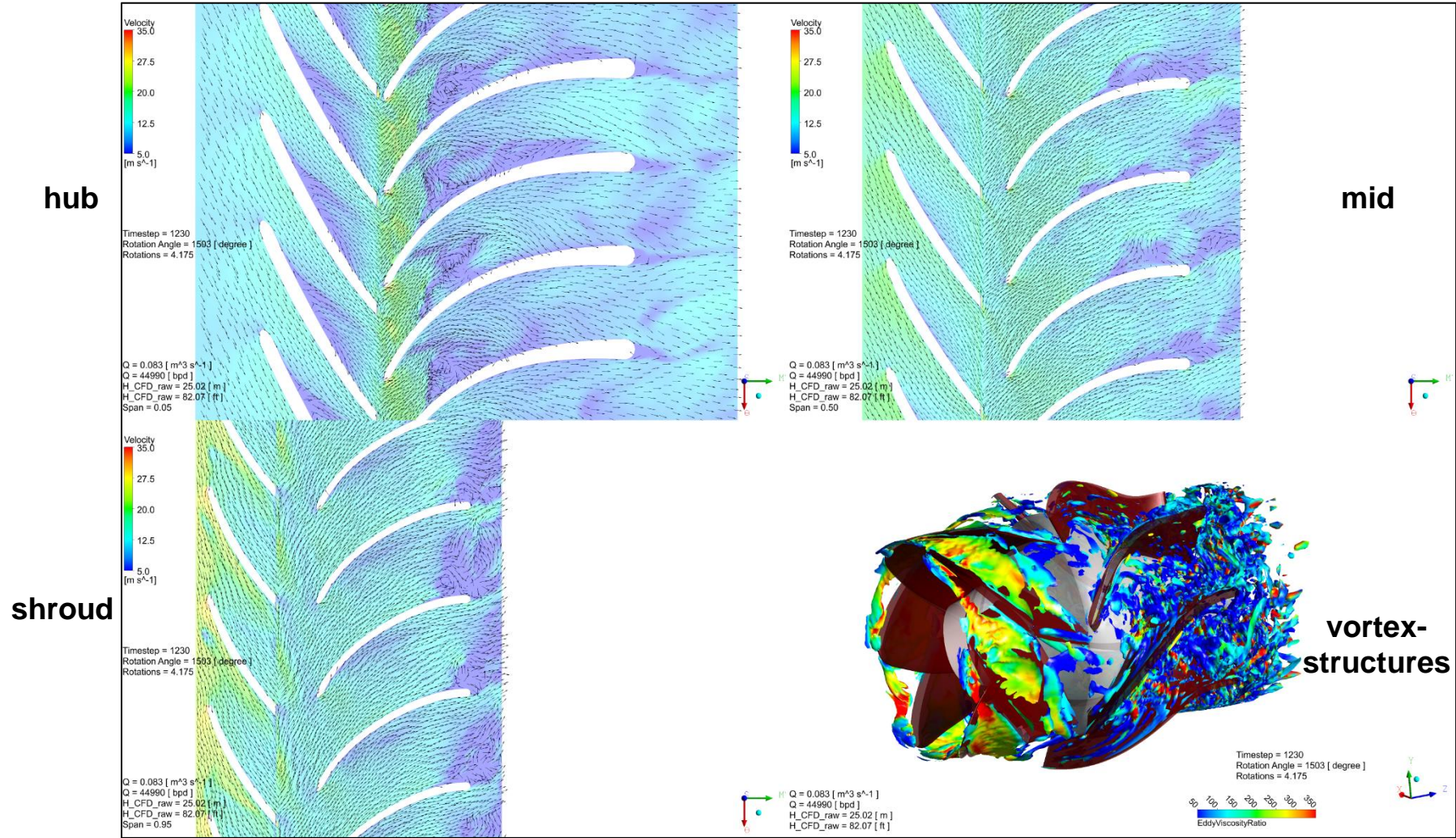
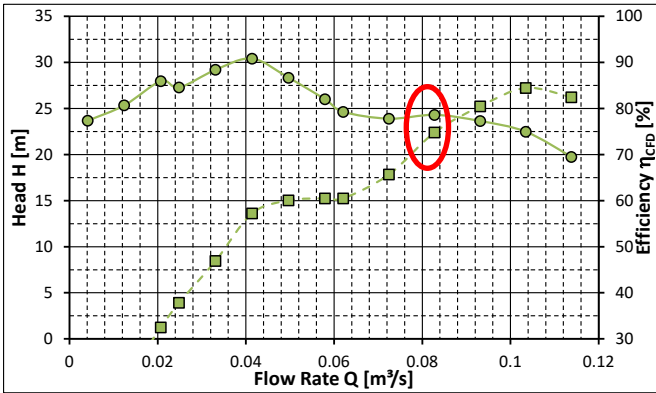
Loss analysis 2 stage-simulation



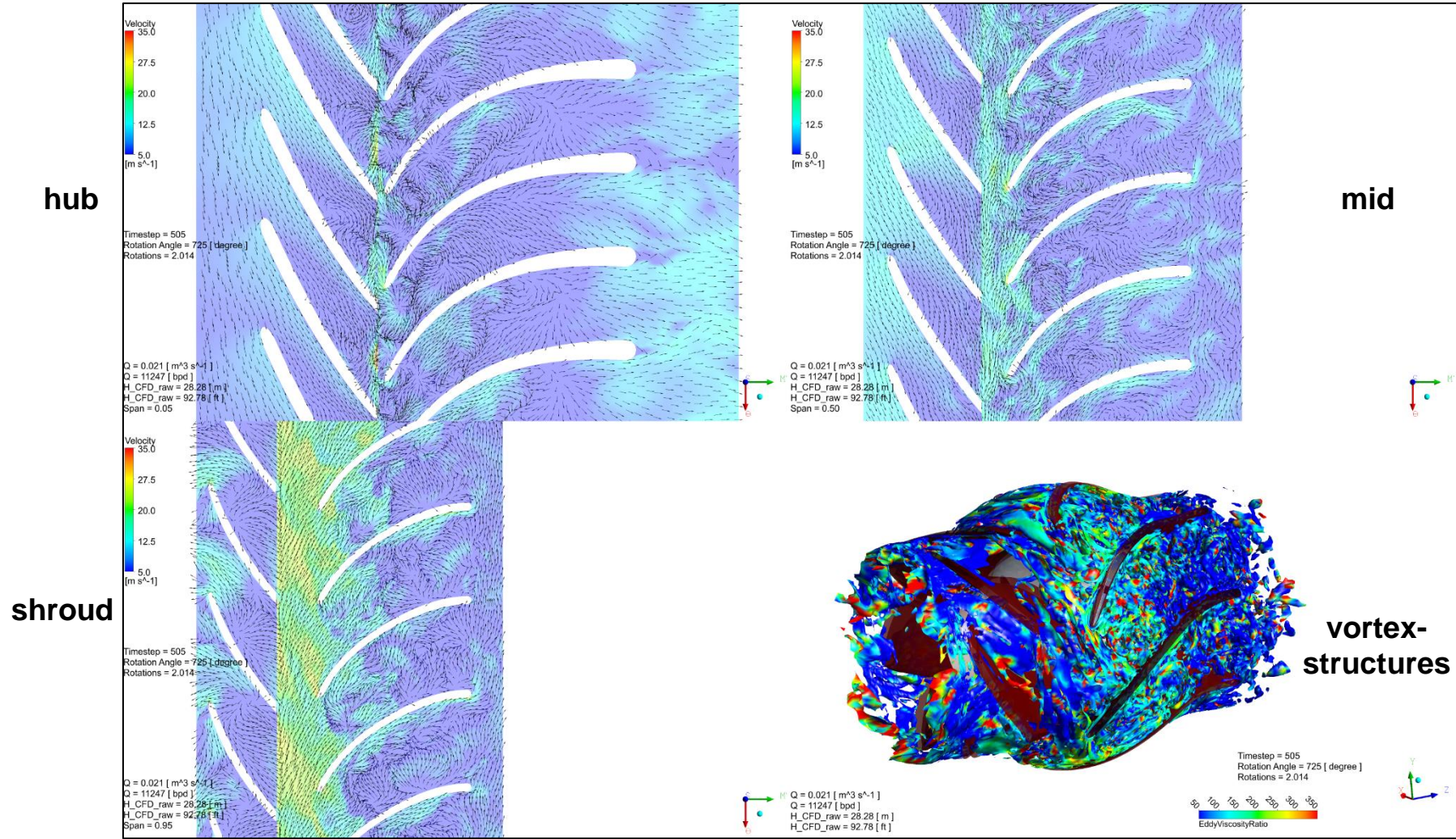
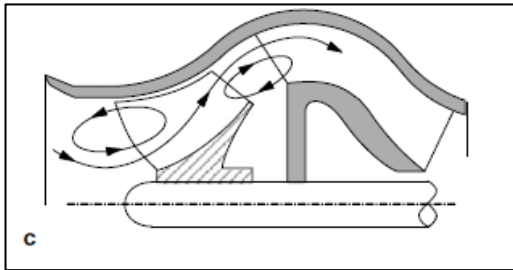
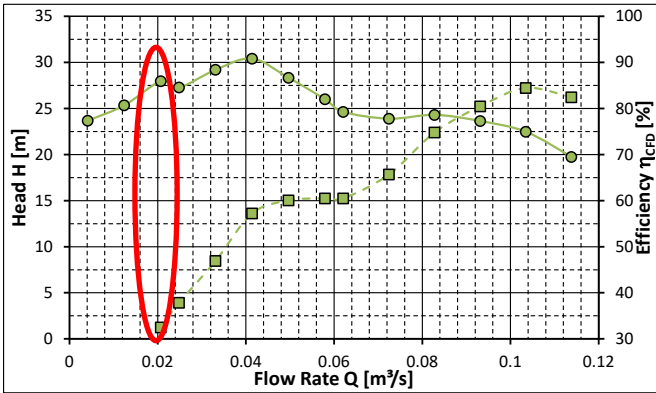
Streamlines reveal strong pre-swirl at part load



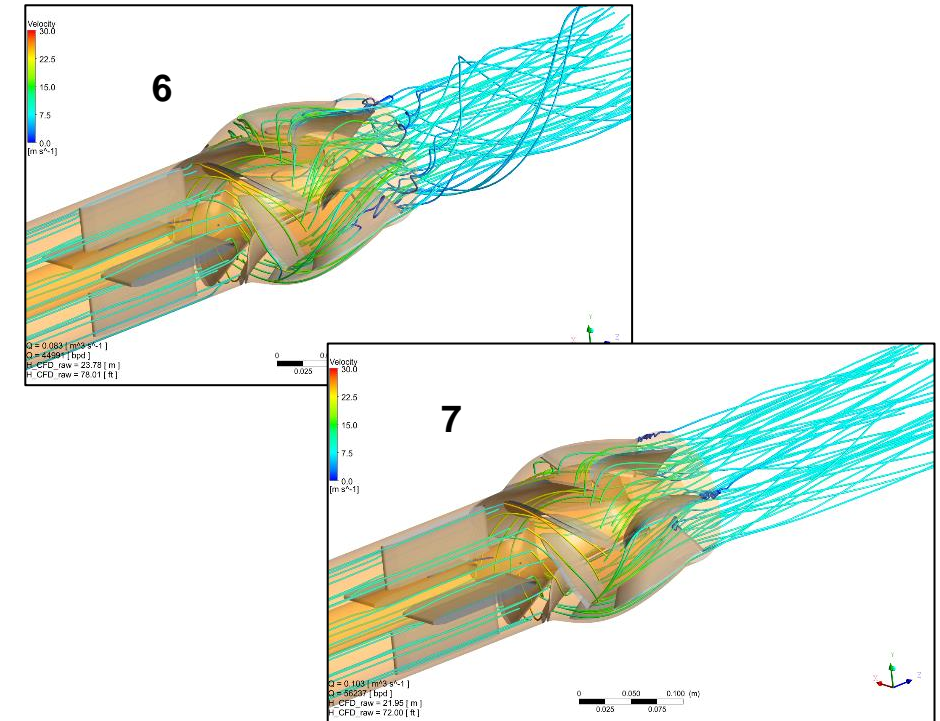
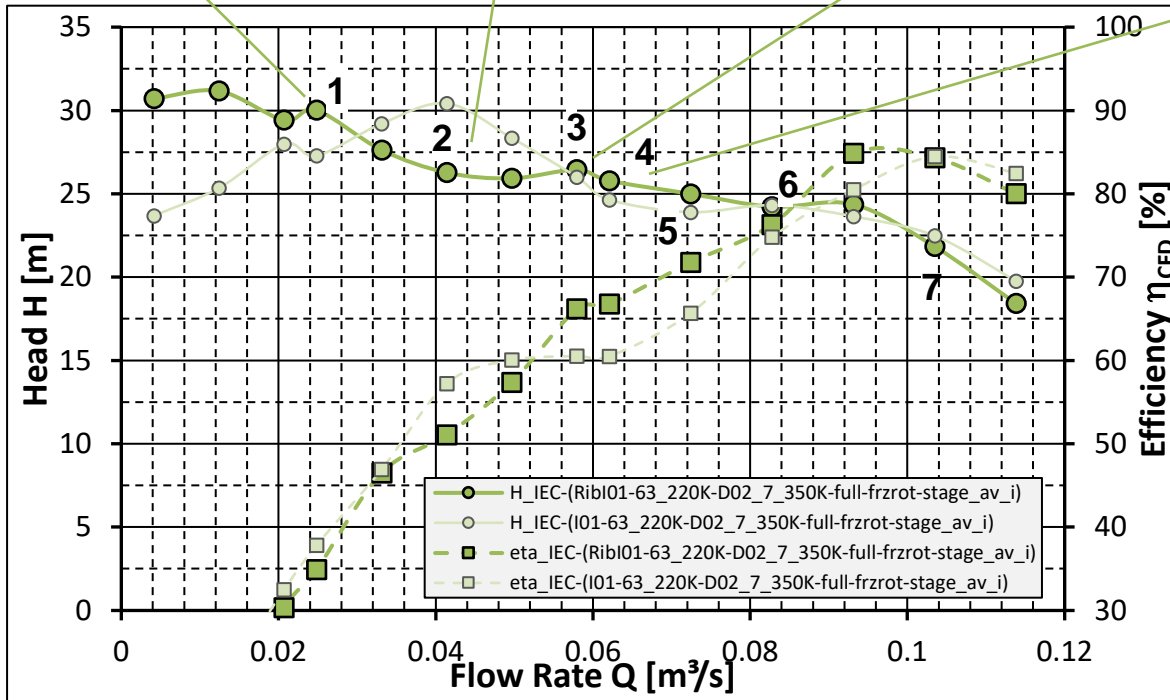
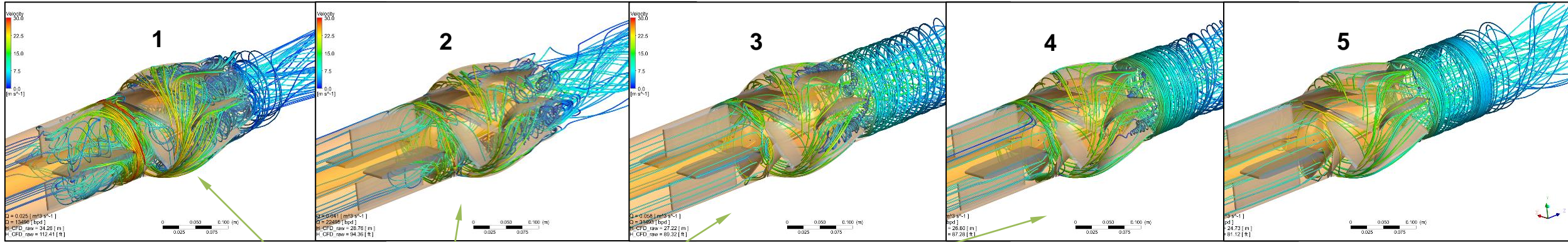
Transient CFD: Q_{Design}



Transient CFD: Part-Load

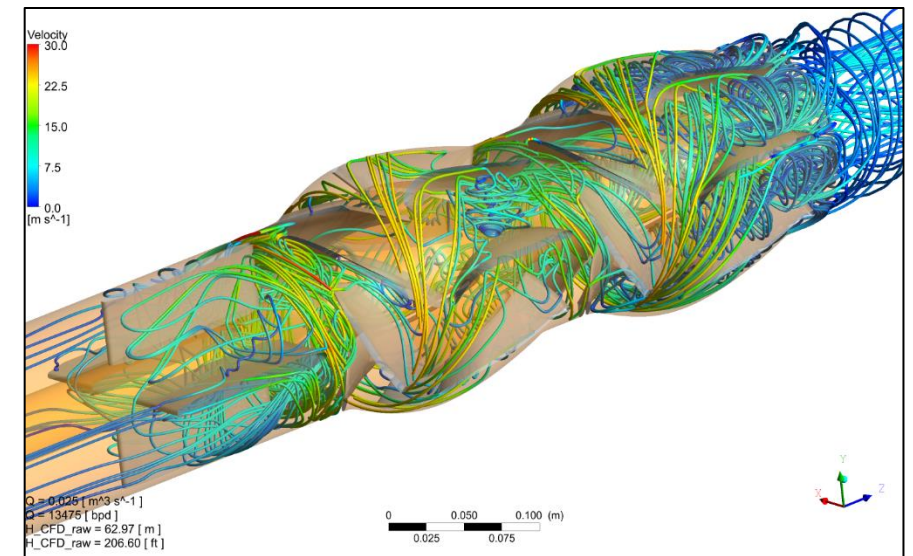
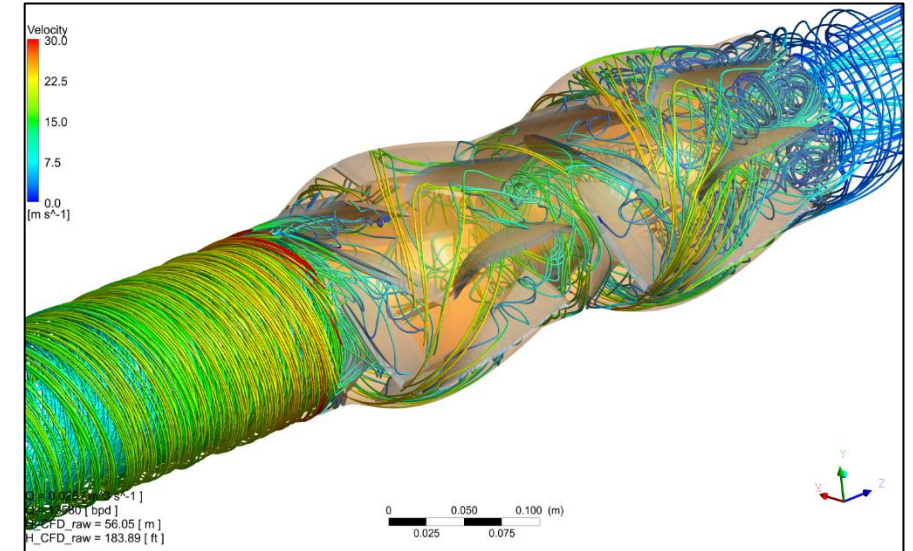


Pre-swirl suppression at part load with flow straightener at inlet



Summary / Outlook: Hydraulic design

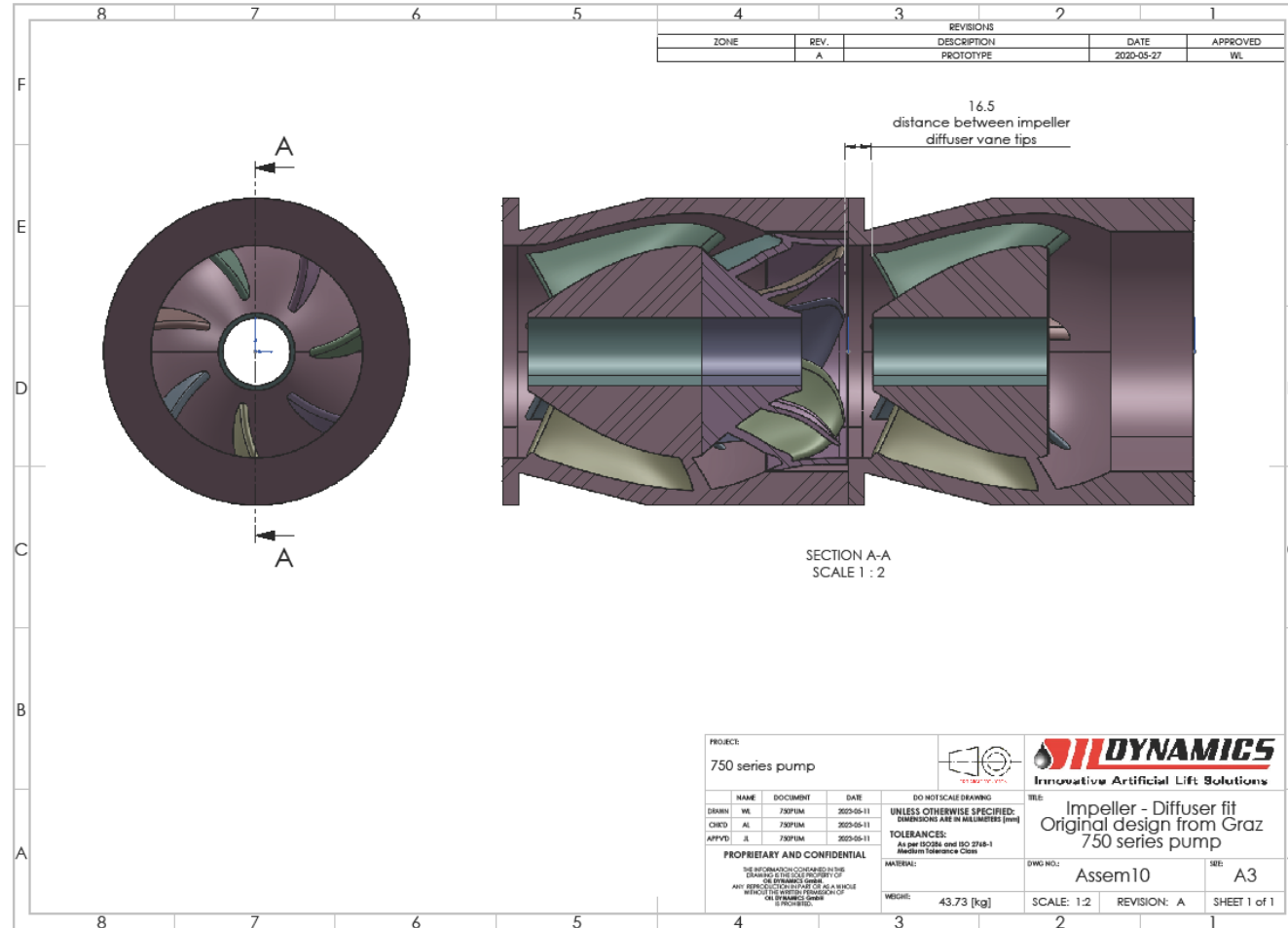
- CFD-results confirm the achievement of the design targets
- Suction recirculation at deep part load was identified to be responsible for head curve instability a flow rates $< 50 \% Q_{\text{Design}}$
 - Simulations with Ribs / Flow straightener showed the successful head curve stabilization when the Part-load swirl can be suppressed
 - In the multi-stage arrangement the diffuser blades will operate as flow straightener for the following stage
 - The ribs in the pump inlet, which are necessary anyway (for reasons of mechanical stability), can serve as flow straighteners for the first pump stage



Production Design – starting model

OD = 190.5mm or 7.5”

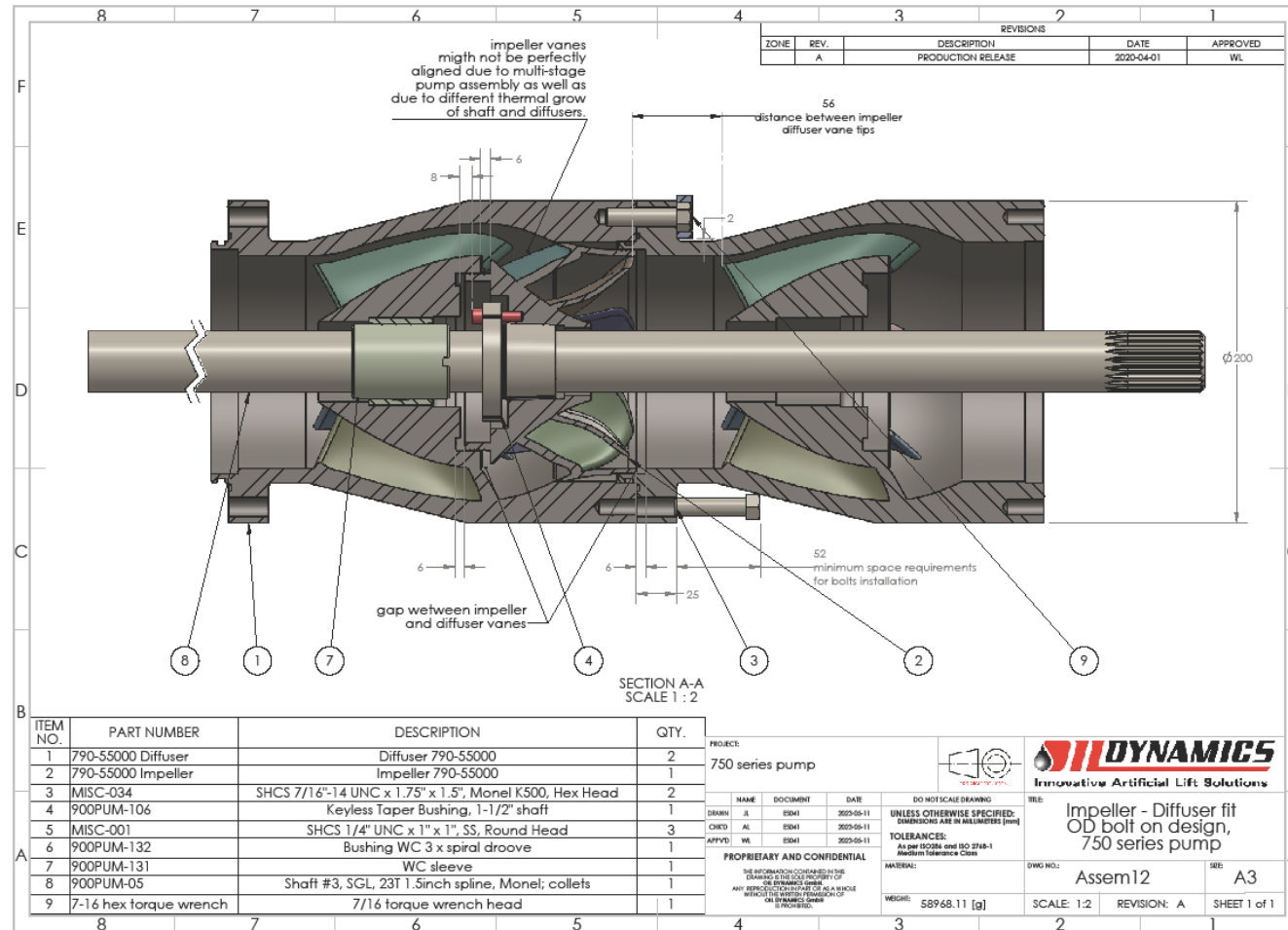
distance between vane tips – 16.5mm



Production Design – step #1

OD = 200mm or 7.87”

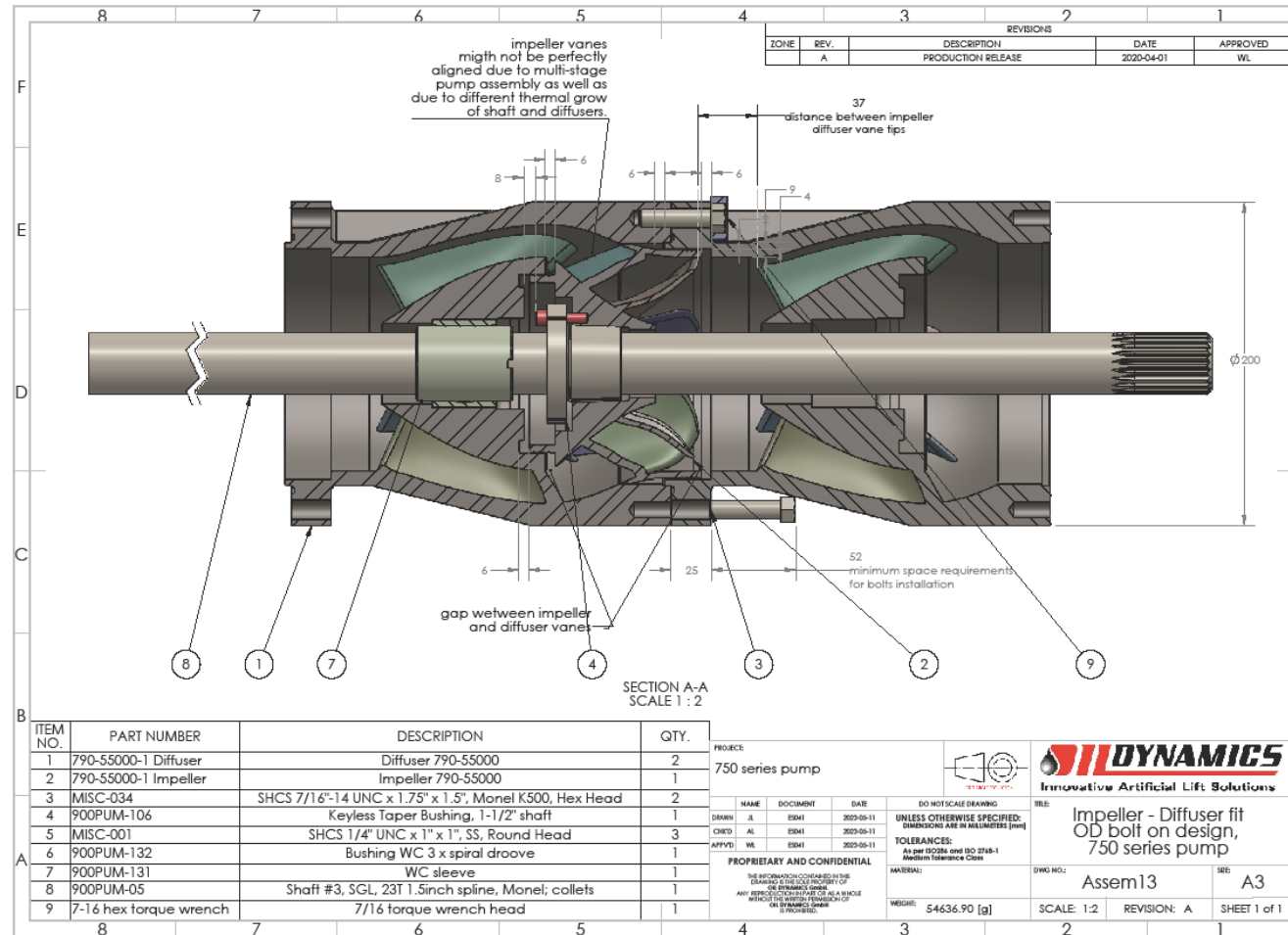
distance between vane tips – 56mm



Production Design – step #2

OD = 200mm or 7.87”

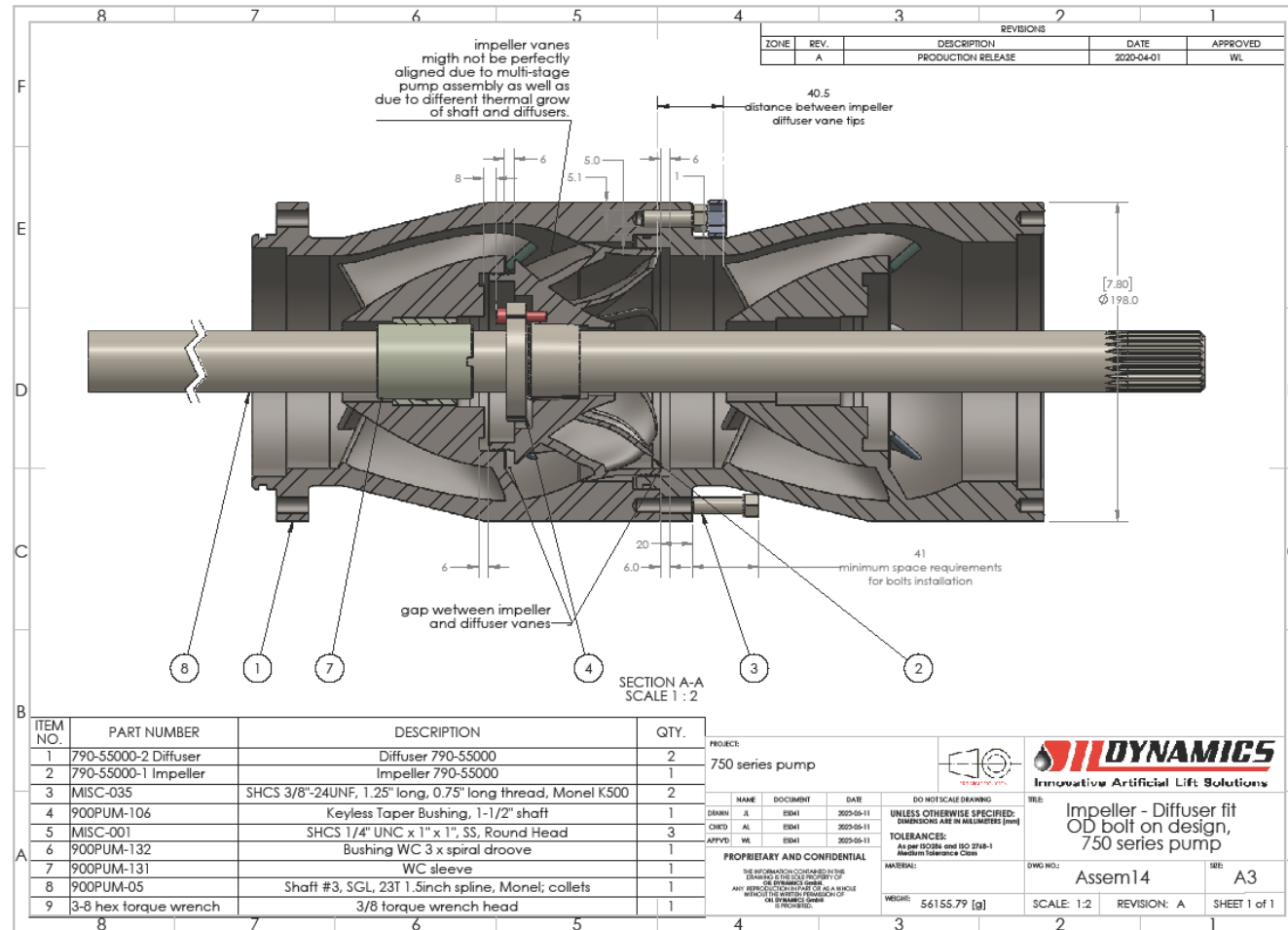
distance between vane tips – 37mm



Production Design – step #3

OD = 200mm or 7.8”

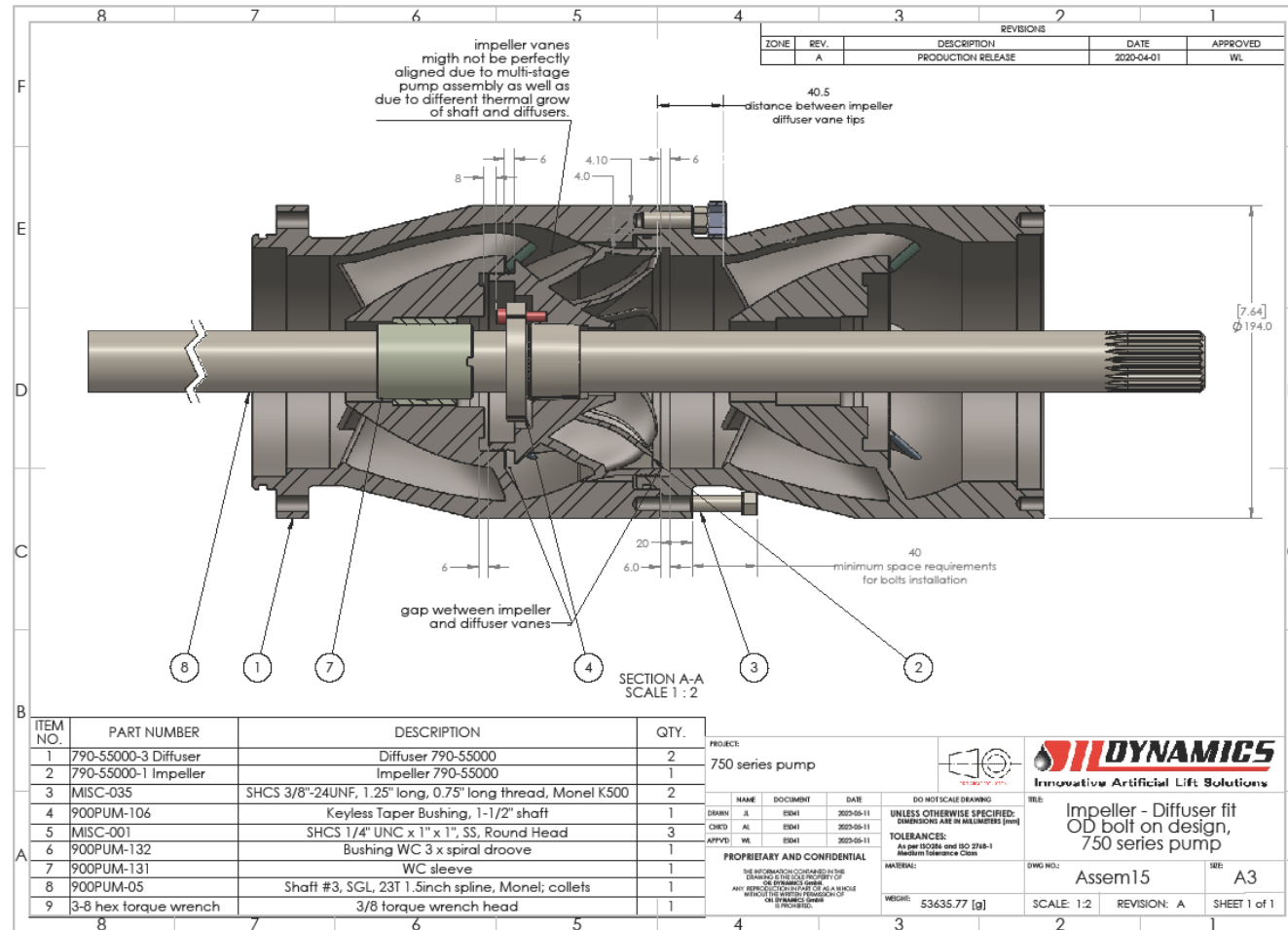
distance between vane tips – 40.5mm



Production Design – step #4

OD = 200mm or 7.64”

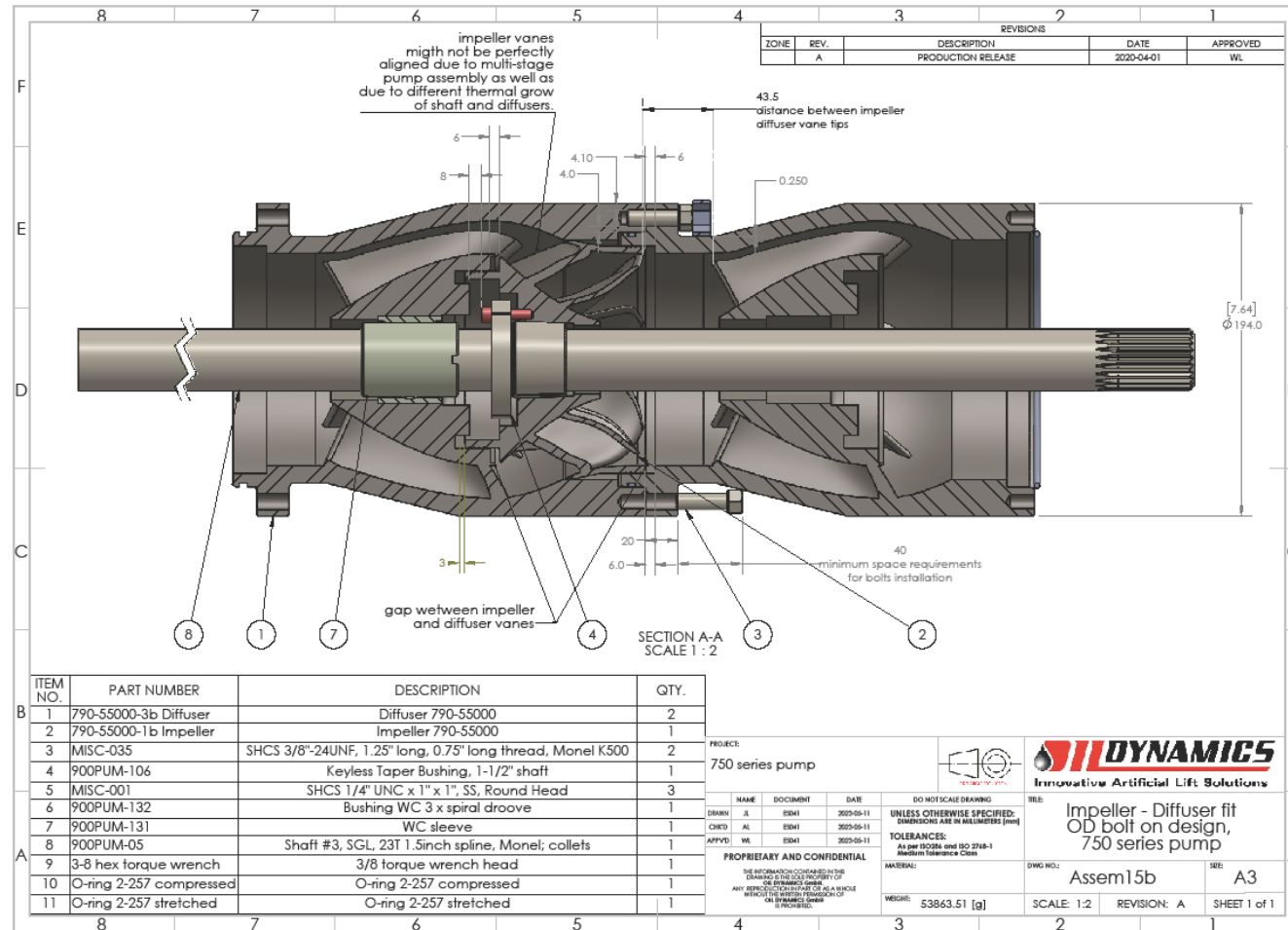
distance between vane tips – 40.5mm



Production Design – step #5

OD = 200mm or 7.64”

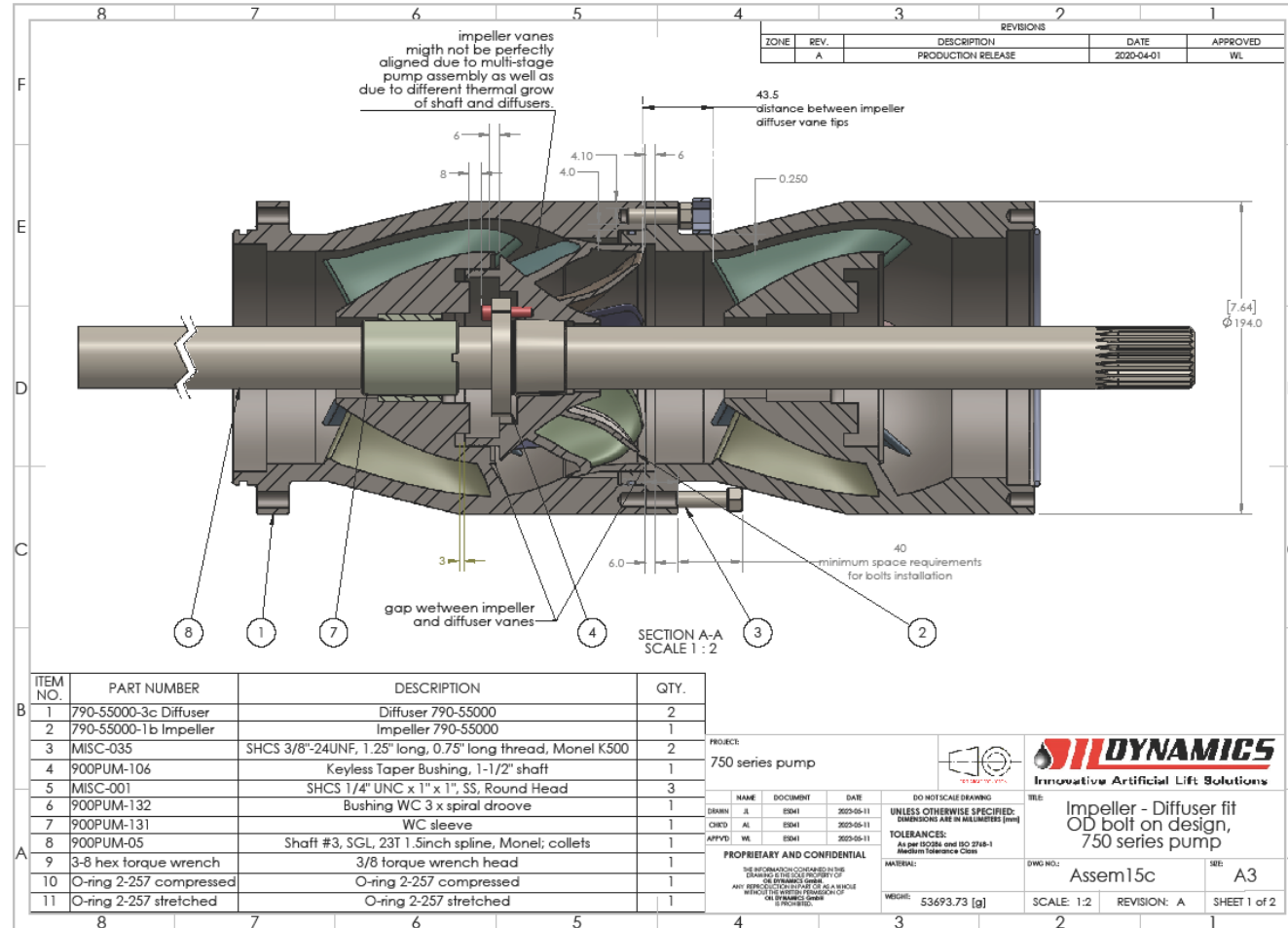
distance between vane tips – 43.5mm



Production Design – step #6

OD = 200mm or 7.64”

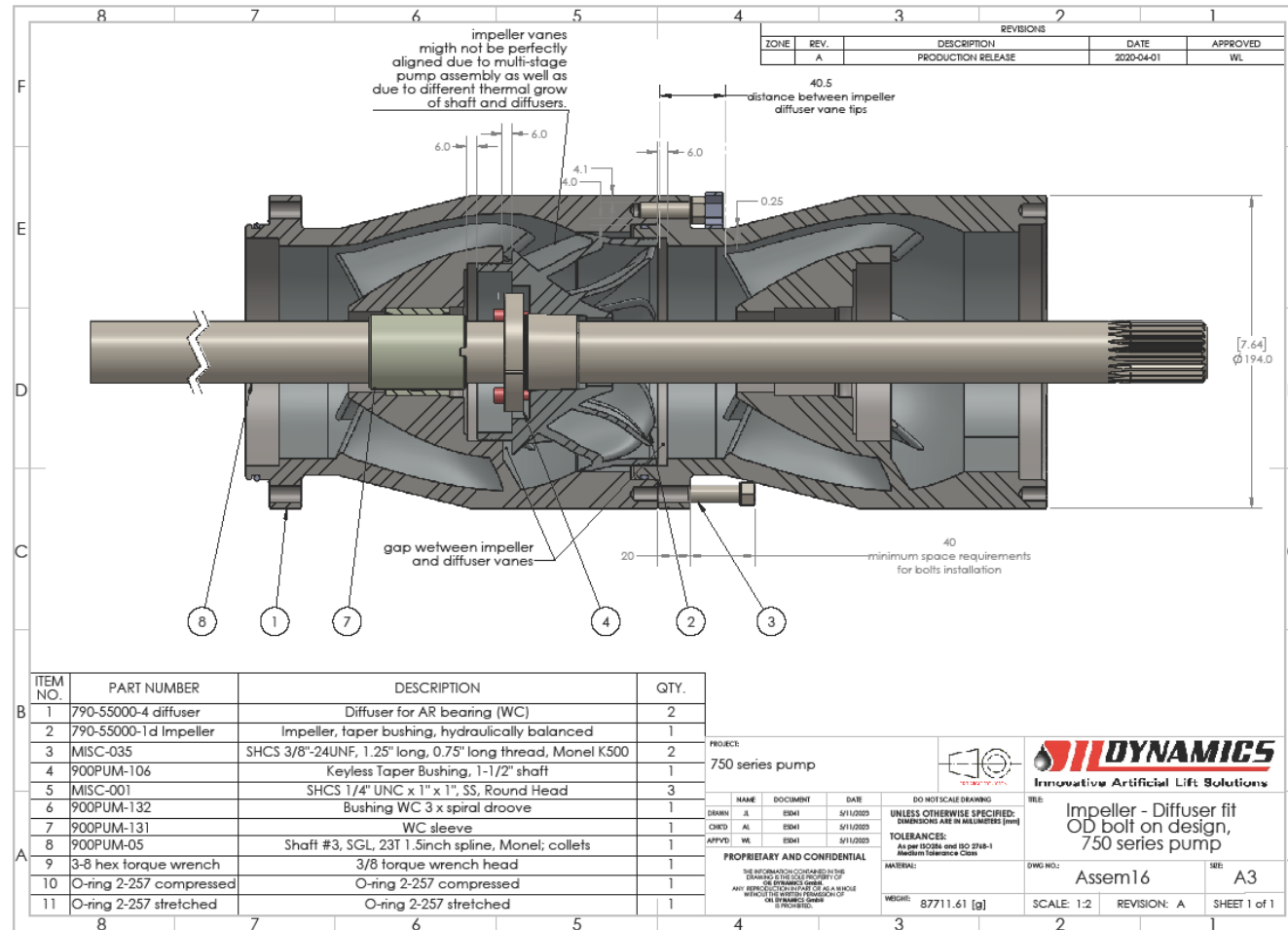
distance between vane tips – 43.5mm



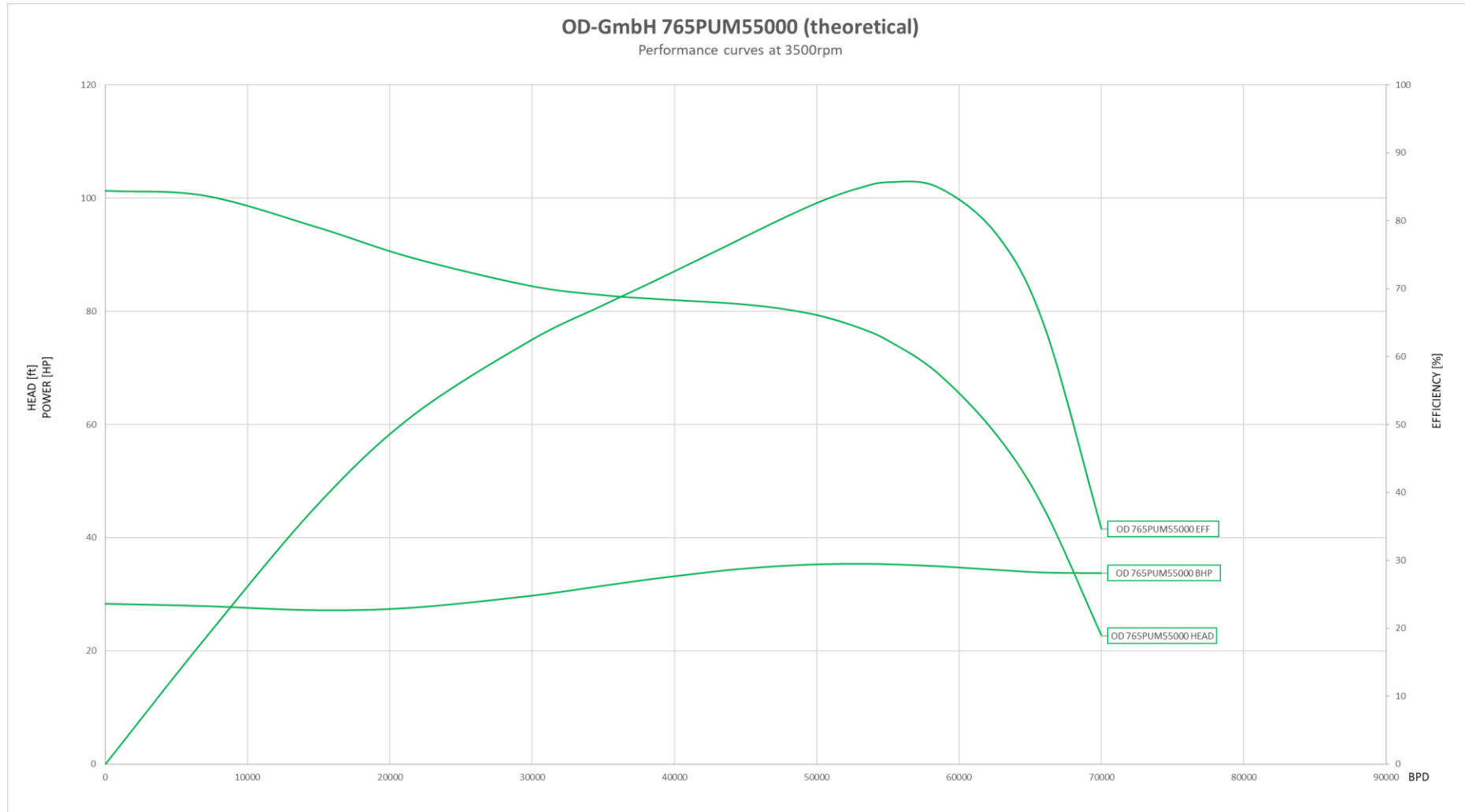
Production Design – Production Release

OD = 200mm or 7.64”

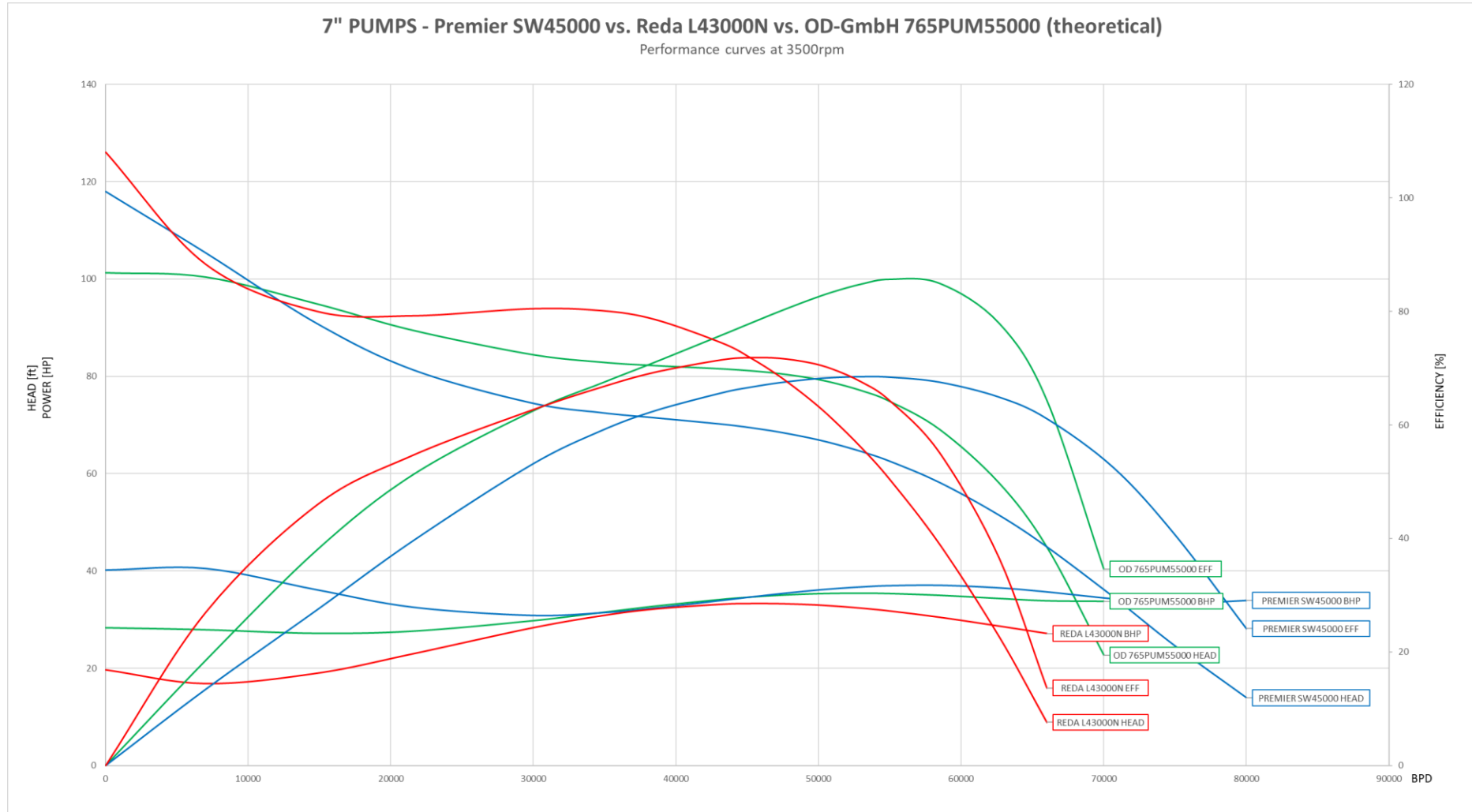
distance between vane tips – 40.5mm



OD-GmbH 765-55000 (theoretical)

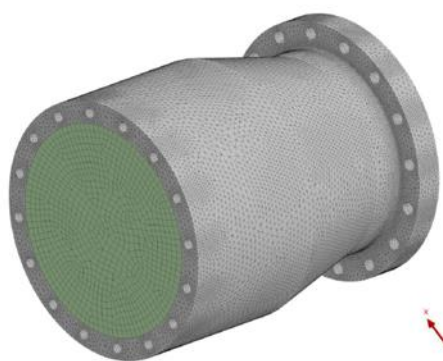
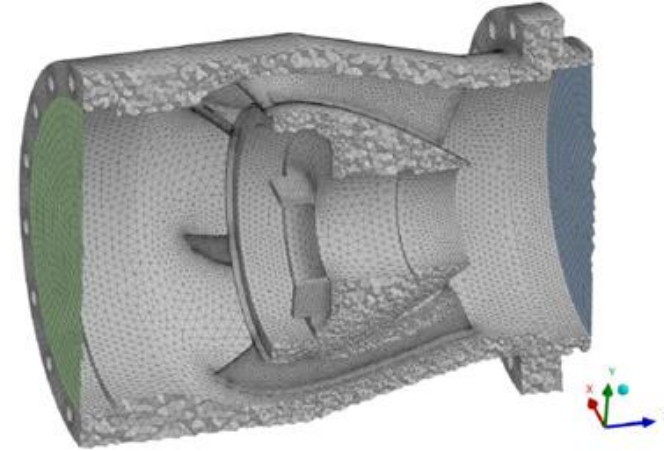


OD-GmbH pump vs. Competition

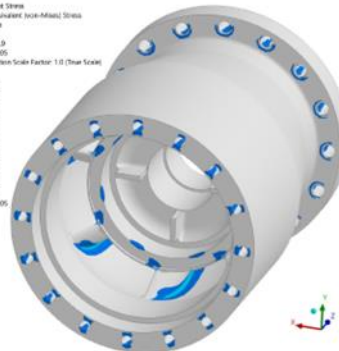


Production Design - FEA

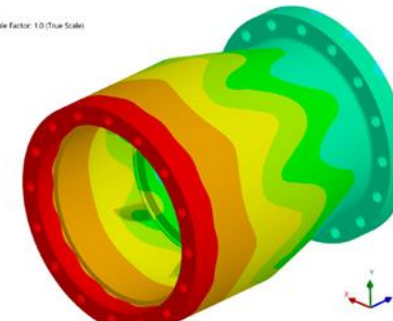
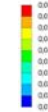
Inner pressure acting on diffuser – 105Bar
Bending moment – 500Nm
Maximum temperature 160°C
Minimum temperature 50°C
Temperature gradient - 110°C
Axial thrust load 120kN
Motor weight below pump – 4T



■ EP8
Equivalent Stress
Type: Equivalent (von-Mises) Stress
Unit: MPa
Time: 1
Max: 984.9
Min: 0.0205
Deformation Scale Factor: 1.0 (True Scale)



■ EP2
Total Deformation
Type: Total Deformation
Unit: mm
Time: 1
Max: 0.043218
Min: 0.01849
Deformation Scale Factor: 1.0 (True Scale)



Production Design

